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ATTORNEY'S DOCKET NO: 010507

U.S. DEPARTMENT OF COMMERCE, PATENT AND TRADEMARK OFFICE		DATE: April 12, 2001
TRANSMITTAL LETTER TO THE UNITED STATES DESIGNATED/ELECTED OFFICE (DO/EO/US) CONCERNING A FILING UNDER 35 U.S.C. 371		U.S. APPL. NO. (if known) 09/806485
INTERNATIONAL APPLICATION NO.: PCT/JP99/05627	INTERNATIONAL FILING DATE: OCTOBER 12, 1999	PRIORITY DATE CLAIMED: OCTOBER 12, 1998
TITLE OF INVENTION: RESIN COMPOSITION AND PROCESS FOR PRODUCING THE SAME		
APPLICANT(S) FOR DO/EO/US: Noriyuki SUZUKI, Tomoya NOMA and Mitsuharu KOUROGI		
Applicant hereby submits to the United States Designated/Elected Office (DO/EO/US) the following items and other information:		
<p>1. <input checked="" type="checkbox"/> This is a FIRST submission of items concerning a filing under 35 U.S.C. 371.</p> <p>2. <input type="checkbox"/> This is a SECOND or SUBSEQUENT submission of items concerning a filing under 35 U.S.C. 371.</p> <p>3. <input checked="" type="checkbox"/> This express request to begin national examination procedures (35 USC 371(f)) at any time rather than delay examination until the expiration of the time limit set in 35 USC 371(b) and PCT Articles 22 and 39(1).</p> <p>4. <input checked="" type="checkbox"/> A proper Demand for International Preliminary Examination was made by the 19th month from the earliest claimed priority date.</p> <p>5. <input checked="" type="checkbox"/> A copy of the International Application as filed (35 U.S.C. 371(c)(2)):</p> <p style="margin-left: 20px;">a. <input type="checkbox"/> is transmitted herewith (required only if not transmitted by the International Bureau).</p> <p style="margin-left: 20px;">b. <input checked="" type="checkbox"/> has been transmitted by the International Bureau.</p> <p style="margin-left: 20px;">c. <input type="checkbox"/> is not required, as the application was filed in the United States Receiving Office (RO/US).</p> <p>6. <input checked="" type="checkbox"/> A translation of the International Application into English (35 U.S.C. 371(c)(2)).</p> <p>7. <input checked="" type="checkbox"/> Amendments to the claims of the International Application under PCT Article 19 (35 U.S.C. 371(c)(3))</p> <p style="margin-left: 20px;">a. <input type="checkbox"/> are transmitted herewith (required only if not transmitted by the International Bureau).</p> <p style="margin-left: 20px;">b. <input type="checkbox"/> have been transmitted by the International Bureau.</p> <p style="margin-left: 20px;">c. <input type="checkbox"/> have not been made; however, the time limit for making such amendments has NOT expired.</p> <p style="margin-left: 20px;">d. <input checked="" type="checkbox"/> have not been made and will not be made.</p> <p>8. <input type="checkbox"/> A translation of the amendments to the claims under PCT Article 19 (35 U.S.C. 371(c)(3)).</p> <p>9. <input type="checkbox"/> An oath or declaration of the inventor(s) (35 U.S.C. 371(c)(4)).</p> <p>10. <input type="checkbox"/> A translation of the annexes to the International Preliminary Examination Report under PCT Article 36 (35 U.S.C. 371(c)(5)).</p> <p>ITEMS 11. TO 16. BELOW CONCERN OTHER DOCUMENT(S) OR INFORMATION INCLUDED:</p> <p>11. <input type="checkbox"/> An Information Disclosure Statement under 37 CFR 1.97 and 1.98.</p> <p>12. <input type="checkbox"/> An assignment document for recording. A separate cover sheet in compliance with 37 CFR 3.28 and 3.31 is included. ASSIGNEE NAME AND ADDRESS: <u>KANEKA CORPORATION, Osaka-shi, Japan</u></p> <p>13. <input type="checkbox"/> A FIRST preliminary amendment. <input type="checkbox"/> A SECOND or SUBSEQUENT preliminary amendment</p> <p>14. <input type="checkbox"/> A substitute specification.</p> <p>15. <input type="checkbox"/> A change of power of attorney and/or address letter.</p> <p>16. <input checked="" type="checkbox"/> Other items or information: International Search Report.</p>		

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U.S. APPLICATION NO. (if known) 09/806485	INTERNATIONAL APPLICATION NO. PCT/JP99/05627	DATE: April 12, 2001	
17. <u>X</u> The following fees are submitted: Basic National Fee (37 CFR 1.492(a)(1)-(5): Search Report has been prepared by the EPO or JPO: \$860.00 International preliminary examination fee paid to USPTO (37 CFR 1.482) \$690.00 No international preliminary examination fee paid to USPTO (37 CFR 1.482) but international search fee paid to USPTO (37 CFR 1.445(a)(2)) \$710.00 Neither international preliminary examination fee (37 CFR 1.482) nor international search fee (37 CFR 1.445(a)(2)) paid to USPTO \$1000.00 International preliminary examination fee (37 CFR 1.482) and all claims satisfied provisions of PCT Article 33(2)-(4) \$100.00 <div style="text-align: right;">ENTER APPROPRIATE BASIC FEE AMOUNT =</div>		CALCULATIONS	PTO USE ONLY
\$ 860.00			
Surcharge of \$130.00 for furnishing the oath or declaration later than <u> </u> 20 <u> </u> x 30 months from the earliest claimed priority date (37 CFR 1.492(e)).		\$ 130.00	
CLAIMS	NUMBER FILED	NUMBER EXTRA	RATE
TOTAL	12 -20 =		X \$ 18.00
INDEPENDENT	1 - 3 =		X \$ 80.00
Multiple dependent claims(s) (if applicable)			+ \$270.00
TOTAL OF ABOVE CALCULATIONS =		\$ 990.00	
Reduction by 1/2 for filing by small entity, if applicable. (Note 37 CFR 1.9, 1.27, 1.28).			
SUBTOTAL =		\$ 990.00	
Processing fee of \$130.00 for furnishing the English translation later than <u> </u> 20 <u> </u> x 30 months from the earliest claimed priority date (37 CFR 1.492(f)). +			
TOTAL NATIONAL FEE =		\$ 990.00	
Fee for recording the enclosed assignment (37 CFR 1.21(h)). The assignment must be accompanied by an appropriate cover sheet (37 CFR 3.28, 3.31). \$40.00 per property +			
TOTAL FEES ENCLOSED =		\$ 990.00	
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a. ☒ A check in the amount of \$ **990.00** to cover the above fees is enclosed. (\$860.00 for filing fee and \$130.00 for late filing of the declaration). (This paper is filed in triplicate)


b. ☐ Please charge my Deposit Account No. 01-2340 in the amount of \$ to cover the above fees. (A duplicate copy of this sheet is enclosed.)

c. ☒ The Commissioner is hereby authorized to charge any additional fees which may be required, or credit any overpayment to Deposit Account No. 01-2340.

NOTE: Where an appropriate time limit under 37 CFR 1.494 or 1.495 has not been met, a petition to revive (37 CFR 1.137(a) or (b)) must be filed to request that the application be restored to pending status.

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DESCRIPTION

RESIN COMPOSITION AND PROCESS FOR PRODUCING THE SAME

5 TECHNICAL FIELD

The present invention relates to a resin composition including polycarbonate resin, polyarylate resin, or thermoplastic polyester resin and silane-treated foliated phyllosilicate, and a method for producing the resin composition.

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BACKGROUND ART

Polycarbonate resin has a good transparency, shock resistance, dimensional accuracy, and heat resistance, and therefore it is widely used in fields of precision machine parts, automobile parts, office automation apparatus parts, and the like. Polyarylate resin has a good heat resistance, transparency, shock resistance, dimensional accuracy, and weather resistance, and therefore it is widely used in fields of electric/electronics parts, precision machine parts, automobile parts, materials for food/medicine, and the like. Thermoplastic polyester resin such as polyethylene terephthalate has a good heat resistance, chemical resistance, weather resistance, mechanical properties, electric characteristics, etc., and therefore it is widely used as a form of, for example, fiber or film in fields of electric/electronics parts, mechanical parts, office automation apparatus parts, electric home appliance parts and the like. All of these resins are being required to have further improved mechanical properties, heat resistance, and the like. For example, the polyarylate resin used for precision machine parts for cameras, watches, etc., is required to have a high level of stiffness, dimensional

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In the light of the above, a variety of fillers, e.g., a fiber-like inorganic substance such as glass fiber, carbon fiber or potassium titanate whisker, or a particle-like inorganic substance such as glass flake, glass bead, talc, mica, or kaolin, etc., has been mixed in the resins. Although mixing inorganic materials certainly improves the mechanical properties, etc. of the resins, it causes a problem of damaging the external appearance of the surface of molded products and increasing the relative density. Furthermore, there was a problem that the orientation of fiber-like inorganic substances causes anisotropy during the injection molding. In addition, for polycarbonate resin and polyarylate resin, there was a problem of damaging the transparency which is a significant feature of these resins.

It has generally been considered that these problems, which may be caused by adding fiber-like inorganic substances or particle-like inorganic substances, result from insufficient dispersion of the inorganic substance and an excessive size of dispersed particles.

Regarding micro-dispersion techniques of inorganic fillers into resins, a variety of techniques are disclosed as follows: (1) a resin composite material including a resin matrix and laminar particles with an average layer thickness of about 50 Å or less and the maximum layer thickness of about 100 Å or less to which an organic metal compound such as an organo-silane compound is bound (International Publication WO95/06090, US Patent

No. 5,514,734, International Publication W093/04118, and International Publication W093/11190); (2) a resin composition in which laminar silicate with an average layer thickness of 25 to 1000 Å and an aspect ratio of 20 to 300 is dispersed in a thermoplastic resin (Japanese Laid-open Publication No. 9-124836; (3) a method for polymerizing a thermoplastic polyester resin after applying a swelling treatment with glycols to a laminar inorganic filler having a layer charge of 0.2 to 1.0 (Japanese Laid-open Publication No. 7-26123); (4) a method for polymerizing a thermoplastic polyester resin after applying a swelling treatment with glycols to an inorganic compound (e.g., swellable fluorine mica) obtained by heating a mixture of talc and alkali silicofluoride (Japanese Laid-open Publication No. 7-268188 and Japanese Laid-open Publication No. 8-73710); (5) a method for polymerizing a thermoplastic polyester resin in an presence of compatibilizing agent and laminar silicate denaturalized with organic onium ion (Japanese Laid-open Publication No. 3-62846); and (6) a method for mixing swellable fluorine mica and proton acid in an arbitrary stage during the polymerizing reaction of a thermoplastic polyester resin (Japanese Laid-open Publication No. 8-120071); and (7) a method for continuously adding a slurry containing 0.1 to 10% by weight of particles having an average grain size of 200 nm or less when a thermoplastic polyester resin is polymerized (Japanese Laid-open Publication No. 9-328538).

The above technique (1) provides a nylon 6 type composite material which consists of nylon 6 and montmorillonite bound with isocyanatepropyl triethoxysilane, etc., copolymerized with caprolactam. It is difficult, however, to obtain a resin composite material

in which laminar particles are micro-dispersed, by directly applying this method using nylon 6 to polycarbonate resin, polyarylate resin or a thermoplastic polyester resin. The above technique (2) uses swellable mica as the laminar silicate, wherein swellable mica swollen with water or alkylammonium-processed swellable mica swollen with xylene is biaxially extruded with polybutyleneterephthalate, etc., whereby a resin composition is obtained. It is difficult, however, to obtain a resin composition having desired properties if this method is directly applied to polyarylate resin or the like, since the micro-dispersion of the laminar silicate is incomplete and heterogeneous. According to each of the above techniques (3) to (7), the micro-dispersion of the laminar silicate in thermoplastic polyester resin is insufficient and therefore it is difficult to obtain a resin composition having desired properties.

In addition to the above problems, for the thermoplastic polyester resin, there has been a problem, in the case where a polyester resin, etc., having a repeating unit of polyalkyleneterephthalate as the fundamental framework is used as a molding material, of the industrial application of the resin being limited since the crystallization rate of the resin is small. For example, if a resin is molded in a common manner in a mold at 100°C or lower, the dimensional stability is significantly deteriorated due to a bad releasability, e.g., the surface quality (surface smoothness) of the molded product is lowered. In addition, it is necessary to extend the retention time in the mold, which results in extending the duration of the molding cycle.

As measures for solving such a problem of crystallization rate, the techniques of adding the following substances as a nucleating agent for crystallization to thermoplastic polyester resin are disclosed: (i) inorganic additives such as talc, mica, silica (Japanese Patent Publication for Opposition No. 46-38707 and Japanese Patent Publication for Opposition No. 47-27142); (ii) copolymer of α -olefin and unsaturated carboxylate (Japanese Patent Publication for Opposition No. 45-26225); and (iii) organic carboxylate such as sodium benzoate (Japanese Patent Publication for Opposition No. 46-29977 and Japanese Laid-open Publication No. 54-158452).

The effects by the above techniques (i) to (iii), i.e., mere addition of nucleating agents for crystallization, are significantly affected by the molding conditions such as the cooling time after filling the resin into the mold and the mold temperature, or the shape of the molded product. Therefore, the crystallization may not sufficiently occur due to these conditions, and sufficient effects cannot be achieved. Furthermore, respective problems arise with each technique: according to the technique (i), it is necessary to add a large quantity of inorganic additives, which causes the decrease of strength, deterioration of color tone or the decrease of surface quality, etc., of the obtained molded product; according to the technique (ii), the decrease of modulus of elasticity occurs; and according to the technique (iii), the decrease of the mechanical properties occurs due to the decrease of the molecular weight of the resin.

The inventors of the present invention obtained a

composite material by introducing laminar particles into polycarbonate and polyarylate resins as a very thin plate-like structure close to the unit layer (the layer thickness of the unit layer is about 10 Å), and performed the evaluation of the physical properties of the composite materials. As a result, it was found that in these composite materials, the mechanical properties and deflection temperature under load were improved compared to the material in which laminar particles were introduced into resin merely as a laminated/aggregated state by using a method such as extrusion, fusion, or kneading. However, it was found that the effects were by no means satisfactory.

This result conforms to the following suggestion in Japanese Laid-open Publication 9-118792. That is, in the case where the laminar particles are separated one by one and dispersed in a form of a molecule in a polypropylene type resin and a vinyl type polymer, the laminar particles form a laminated structure and are not likely to express the isotropic properties (Nendo Kagaku, vol. 30(2), 143-147 (1990)). Furthermore, laminar particles *per se* naturally have a high modulus of elasticity, and if they are separated so as to be in a state close to the unit layer, they are distorted and cannot provide a normally expected modulus of elasticity.

As described above, by merely dispersing the laminar silicate in a resin matrix so that the laminar silicate has an average layer thickness of about 50 Å or less and the maximum layer thickness of about 100 Å or less, which is a state close to the unit layer, or by introducing the laminar silicate into the resin matrix merely in a laminated/aggregated state, it is difficult to obtain, by

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either method, a resin composition having sufficiently improved properties. Therefore, techniques have been sought for dispersing laminar particles having an appropriate layer thickness in resin composition so as to provide the resin composition with a variety of positive properties. An object of the present invention is to provide such techniques.

Regarding thermoplastic polyester resin, the inventors of the present invention disclosed in International Publication W097/43343, a technique of utilizing a silane-treated foliated phyllosilicate in which an organo-silane compound is introduced into layered swellable silicate. By polymerizing diol slurry containing the clay composite and a diol compound such as bishydroxyalkylterephthalate as essential components, the laminar particles are micro-dispersed in the thermoplastic polyester resin, thereby providing a polyester resin composition with an improved mechanical properties, and so on. However, the preparation of the above diol slurry requires significant time and effort, and therefore imposes a problem which causes a high cost, and therefore improvements have been sought. Another object of the present invention is to solve such a conventional problem.

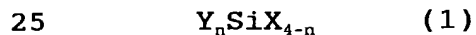
Regarding thermoplastic polyester resins, there is also the problem of crystallization rate as described above, and therefore techniques for improvements in the moldability such as releasability and the molding cycle of thermoplastic polyester resins regardless of the molding conditions and the shape of the product have been sought. A further object of the present invention is to solve such a conventional problem.

DISCLOSURE OF THE INVENTION

In order to achieve the above objects, the inventors
5 of the present invention have conducted diligent studies.
As a result, they found that a significantly improved resin
composition can be obtained by preparing a silane-treated
foliated phyllosilicate by introducing an organo-silane
10 compound into a swellable silicate which was separated and
exfoliated so as to have an appropriate layer thickness,
and homogeneously dispersing the silane-treated foliated
phyllosilicate into the resin, in a state in which the
silane-treated foliated phyllosilicate is fractionated as
15 a submicroscopic thin plate-shape, thereby completing the
present invention.

The composition provided by the present invention
is a resin composition comprising: a resin and a
silane-treated foliated phyllosilicate,

20 wherein the resin is selected from the group
consisting of polycarbonate, polyarylate, and
thermoplastic polyester, and the silane-treated foliated
phyllosilicate is prepared by introducing an organo-silane
compound represented by a general formula (1):



(where n is an integer from 0 to 3; Y is a hydrocarbon
group with 1 to 25 carbons; the hydrocarbon group may have
a substituent(s); X is a hydrolyzable group or hydroxyl
group; n Ys may be the same type or different types; and
30 (4-n) Xs may be the same type or different types) into a
swellable silicate, and wherein at least one of the following
conditions (a) and (b) is satisfied:

(a) an average layer thickness of the silane-

treated foliated phyllosilicate is 500 Å or less; and

(b) [N] value is 30 or more (where the [N] value is defined as the number of particles per a unit weight ratio of the silane-treated foliated phyllosilicate contained in an area of 100 μm^2 of the resin composition) and an average aspect ratio is 10 to 300 (where the average aspect ratio is defined as an average of a ratio of a layer length to a layer thickness of the silane-treated foliated phyllosilicate),

and wherein in the case where the resin is a thermoplastic polyester, at least one of the following conditions (i) to (iii) is further satisfied:

(i) a difference ($\eta_e - 3\eta$) between an extensional viscosity η_e and the triple value of a shear viscosity η of the resin composition is 300 Pa's or more at a temperature of 280°C and a rate of strain of 100 (1/s);

(ii) between a rate of strain of 100 (1/s) and a rate of strain of 1000 (1/s), a difference ($\Delta\eta_e$) of values of the extensional viscosity η_e of the resin composition at a temperature of 280°C is 500 Pa's or more; and

(iii) a product $J_{e0}\eta_0$ of equilibrium compliance J_{e0} and zero shear viscosity η_0 of the resin composition at a temperature of 280°C is 0.8 seconds or more.

In one embodiment, the above-described resin is polycarbonate.

In one embodiment, the above-described resin is polyarylate.

In one embodiment, the above-described resin is thermoplastic polyester.

In one embodiment, the polyester resin composition is a resin composition in which all the above-described conditions (i) to (iii) are satisfied.

5 In one embodiment, the average layer thickness of the above-described silane-treated foliated phyllosilicate is 500 Å or less and the maximum layer thickness is 2000 Å or less.

10 In one embodiment, when the average layer thickness of the above-described silane-treated foliated phyllosilicate is 500 Å or less and the maximum layer thickness is 2000 Å or less, the [N] value is 30 or more.

15 In one embodiment, when the average layer thickness of the above-described silane-treated foliated phyllosilicate is 500 Å or less and the maximum layer thickness is 2000 Å or less, the average aspect ratio is 10 to 300.

20 The method provided by the present invention is a method for producing the above-described resin composition, comprising the steps of:

 (A) preparing a clay dispersion including the
25 above-described silane-treated foliated phyllosilicate and a dispersion medium;

 (B) mixing a polymerizable prepolymer and the clay dispersion; and

 (C) forming the resin by polymerizing the
30 polymerizable prepolymer,

 wherein, in the case where the resin is a thermoplastic polyester, the clay dispersion comprises a dispersion medium containing water in the step (A).

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In one embodiment, a basal spacing of the silane-treated foliated phyllosilicate in the clay dispersion prepared in the step (A) is the three times or more larger than the initial basal spacing of the above-described swellable silicate.

In one embodiment, the above-described resin composition is for an injection molding. The composition for injection molding is preferably a polyester resin composition.

BEST MODE FOR CARRYING OUT THE INVENTION

Hereinafter, the present invention will be described in more detail.

(Polycarbonate resin)

The polycarbonate resin used in the present invention is not specifically limited, and includes all of aliphatic, alicyclic, and aromatic polycarbonates. Among these, aromatic polycarbonates are preferable. An aromatic polycarbonate can be produced by the reaction between one or more bisphenols which may contain polyhydric phenols and carbonic acid esters such as bisalkylcarbonate, bisarylcarbonate, and phosgene.

Bisphenols include, specifically, bis(4-hydroxyphenyl)methane; 1,1-bis(4-hydroxyphenyl)ethane; 1,1-bis(4-hydroxyphenyl)propane; 2,2-bis(4-hydroxyphenyl)propane, i.e., bisphenol A; 2,2-bis(4-hydroxyphenyl)butane; 2,2-bis(4-hydroxyphenyl)pentane; 2,2-bis(4-hydroxyphenyl)-3-methylbutane; 2,2-bis(4-

hydroxyphenyl)hexane; 2,2-bis(4-hydroxyphenyl)-4-
 methylpentane; 1,1-bis(4-hydroxyphenyl)cyclopentane,
 1,1-bis(4-hydroxyphenyl)cyclohexane; bis(4-hydroxy-3-
 methylphenyl)methane; bis(4-hydroxy-3-
 5 methylphenyl)phenylmethane; 1,1-bis(4-hydroxy-3-
 methylphenyl)ethane; 2,2-bis(4-hydroxy-3-
 methylphenyl)propane; 2,2-bis(4-hydroxy-3-
 ethylphenyl)propane; 2,2-bis(4-hydroxy-3-
 isopropylphenyl)propane; 2,2-bis(4-hydroxy-3-sec-
 10 butylphenyl)propane; bis(4-hydroxyphenyl)phenylmethane;
 1,1-bis(4-hydroxyphenyl)-1-phenylethane; 1,1-bis(4-
 hydroxyphenyl)-1-phenylpropane; bis(4-
 hydroxyphenyl)diphenylmethane; bis(4-
 hydroxyphenyl)dibenzylmethane; 4,4'-
 15 dihydroxydiphenylether; 4,4'-dihydroxydiphenylsulfone;
 4,4'-dihydroxydiphenylsulfide; 4,4'-
 dihydroxybenzophenone; phenolphthalein; and the like. The
 most typical phenol among these is bisphenol A.

20 Although there is no limitation to the method for
 producing the polycarbonate resin used for the present
 invention, the following methods are generally known: an
 interfacial polymerization method in which an alkali metal
 salt of bisphenols and a nucleophilic attack-active
 25 derivative of carbonic acid ester are used as raw material
 and they are subjected to a polycondensation reaction at
 the interface between an organic solvent dissolving the
 resultant polymer and alkali water; a pyridine method in
 which bisphenols and a nucleophilic attack-active
 30 derivative of carbonic acid ester are used as raw materials
 and they are subjected to a polycondensation reaction in
 an organic base such as pyridine; and a transesterification
 method in which bisphenols and a carbonic acid ester such

as bisalkylcarbonate or bisarylcarbonate are used as raw materials and a polycarbonate is formed by transesterification reaction. Examples of the nucleophilic attack-active derivative of carbonic acid ester used in the interfacial polymerization method and the pyridine method include phosgene, carbodiimidazole, and the like, among which phosgene is the most commonly used since it is easy to obtain. Specific examples of carbonic acid esters used in the transesterification method include: dimethylcarbonate, diethylcarbonate, di-n-propylcarbonate, diisopropylcarbonate, and di-n-butylcarbonate, etc., as bis-alkylcarbonates; and diphenylcarbonate, bis(2,4-dichlorophenyl)carbonate, bis(2,4,6-trichlorophenyl)carbonate, bis(2-nitrophenyl)carbonate, bis(2-cyanophenyl)carbonate, bis(4-methylphenyl)carbonate, bis(3-methylphenyl)carbonate, dinaphthylcarbonate, etc., as bisarylcarbonates. Among these, dimethylcarbonate, diethylcarbonate, and diphenylcarbonate are most preferably used since their raw materials are easy to obtain and the reaction readily occurs. The above polycarbonate resins may be used alone or in a combination of two or more kinds having different compositions or components and/or different molecular weights.

Although there is no specific limitation to the molecular weight of the polycarbonate resins used in the present invention, the weight average molecular weight M_w measured at 40°C by gel permeation chromatography (GPC) with tetrahydrofuran (THF) solvent, for example, is typically 15,000 to 80,000, and preferably 30,000 to 70,000 in terms of monodisperse polystyrene. If M_w is less than 15,000, the mechanical properties and shock resistance of the molded

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Among the above aromatic dicarboxylic acids, terephthalic acid, isophthalic acid, 2,6-naphthalenedicarboxylic acid, 4,4'-biphenyldicarboxylic acid, and ester-formable derivatives thereof are preferable because of their mechanical properties and easy obtainability.

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(2)

The chemical structure (2) depicts a biphenyl core where two benzene rings are connected by a central 'A' group. The left benzene ring has a hydroxyl group (HO-) at the 4-position and is substituted with R¹ at the 1-position, R² at the 2-position, R³ at the 3-position, and R⁴ at the 6-position. The right benzene ring has a hydroxyl group (-OH) at the 4-position and is substituted with R⁵ at the 1-position, R⁶ at the 2-position, R⁷ at the 3-position, and R⁸ at the 6-position. The 'A' group represents a variable linker between the two rings.

(wherein: -A- is -O-, -S-, -SO-, -SO₂-, -CO-, an alkylene group containing 1 to 20 carbons or an alkylidene group containing 6 to 20 carbons; R¹, R², R³, R⁴, R⁵, R⁶, R⁷, and R⁸ are either hydrogen atom, halogen atom, or monovalent hydrocarbon group containing 1 to 5 carbons; and R¹ to R⁸ may

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be the same or different). Examples of the bisphenol compounds include 2,2-bis(4-hydroxyphenyl)propane ("bisphenol A"); bis(4-hydroxyphenyl)methane; 1,1-bis(4'-hydroxyphenyl)ethane; 1,1-bis(4-hydroxyphenyl)-
5 3,3,5-trimethylcyclohexane ("bisphenol TMC"); bis(4-hydroxyphenyl)cyclohexylmethane; 2,2-bis(4'-hydroxy-3,5'-dibromophenyl)propane; bis(4-hydroxy-3,5-dichlorophenyl)methane; bis(4-hydroxy-3,5-dimethylphenyl)methane; 2,2-bis(4'-hydroxy-3',5'-
10 dimethylphenyl)propane; 1,1-bis(4'-hydroxyphenyl)-1-phenylethane; 4,4'-dihydroxydiphenylether; bis(4-hydroxy-3,5-dimethylphenyl)ether; bis(4-hydroxyphenyl)sulfone; bis(4-hydroxy-3,5-dimethylphenyl)sulfone; 4,4'-dihydroxybenzophenone and
15 bis(4-hydroxyphenyl)sulfide, etc. Substituted products and derivatives thereof can also be used. Two or more kinds of these may be mixed and used. It is also possible to use, in combination, aliphatic glycols such as ethylene glycol, propylene glycol, butylene glycol, hexylene glycol,
20 neopentyl glycol, alicyclic glycols such as 1,4-cyclohexanedimethanol, alkylene oxide-addition polymer of bisphenols (e.g., ethylene oxide-addition polymer of bisphenol A), etc., if they are used in a small amount so as not to significantly reduce the features of the
25 polyarylate resin.

Among the above diphenols, 2,2-bis(4-hydroxyphenyl)propane ("bisphenol A"); bis(4-hydroxy-3,5-dimethylphenyl)methane; 2,2-bis(4-hydroxy-3,5-dimethylphenyl)propane; 1,1-bis(4-hydroxyphenyl)-3,3,5-trimethylcyclohexane ("bisphenol TMC") are preferable
30 because of their handling ability and mechanical properties.

Therefore, the specific examples of the polyarylate resins used in the present invention are the polyarylate resins obtained by reacting any combination of the aromatic dicarboxylic acids and diphenols listed above. Among these, the following combination is preferable because of the mechanical properties and cost, etc.: polyarylate obtained by the reaction between terephthalic acid and 2,2-bis(4-hydroxyphenyl)propane ("bisphenol A") (e.g., trade name: U polymer, Unitika Ltd.); polyarylate obtained by the reaction between isophthalic acid and 2,2-bis(4-hydroxyphenyl)propane (e.g., trade name: Arylon, Du Pont); polyarylate obtained by the reaction between the mixture of terephthalic acid and isophthalic acid and 2,2-bis(4-hydroxyphenyl)propane; polyarylate obtained by the reaction between the mixture of terephthalic acid and isophthalic acid and the mixture of 2,2-bis(4-hydroxyphenyl)propane and 1,1-bis(4-hydroxyphenyl)-3,3,5-trimethylcyclohexane; polyarylate obtained by the reaction between the mixture of isophthalic acid and 2,5-naphthalenedicarboxylic acid and 2,2-bis(4-hydroxyphenyl)propane; polyarylate obtained by the reaction between the mixture of isophthalic acid and 2,5-naphthalenedicarboxylic acid and the mixture of 2,2-bis(4-hydroxyphenyl)propane and 1,1-bis(4-hydroxyphenyl)-3,3,5-trimethylcyclohexane; and polyarylate resin produced using two or more kinds of aromatic dicarboxylic acids and/or diphenols used for producing these resins. The above polyarylate resins can be used alone, or in a combination of two or more kinds which have different compositions or components and/or different molecular weights.

Although there is no specific limitation to the molecular weight of the polyarylate resins, for example, the weight average molecular weight (Mw) measured at 25°C by gel permeation chromatography (GPC) using chloroform is typically 15,000 to 80,000, and preferably 30,000 to 70,000 in terms of monodisperse polystyrene. If Mw is less than 15,000, the mechanical properties of the obtained polyarylate resin composition tends to be reduced, and if Mw is more than 80,000, the moldability is likely to be reduced.

(Thermoplastic polyester resin)

The thermoplastic polyester resin used in the present invention is any of conventionally known thermoplastic polyester resins obtained by the reaction between a dicarboxylic acid compound and/or an ester-formable derivative of dicarboxylic acid and a diol compound and/or an ester-formable derivative of a diol compound.

For the above dicarboxylic compound, an aromatic dicarboxylic acid is preferable. Examples thereof include: terephthalic acid, isophthalic acid, orthophthalic acid; 2,6-naphthalenedicarboxylic acid; 4,4'-biphenyldicarboxylic acid; 4,4'-diphenyletherdicarboxylic acid; 4,4'-diphenylmethanedicarboxylic acid; 4,4'-diphenylsulfonedicarboxylic acid; 4,4'-diphenylisopropylidenedicarboxylic acid, and the like. Substituted compounds thereof (e.g., an alkyl substituted compound of methylisophthalic acid, etc.) and ester-formable derivatives thereof (e.g., alkyl ester compounds such as terephthalic acid dimethyl, or 2,6-naphthalenedicarboxylic acid dimethyl) can also be used. Aromatic oxyacids such as p-oxybenzoate and p-

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furthermore preferably 0.40 to 1.8 (dl/g). If the logarithmic viscosity is less than 0.3 (dl/g), the mechanical properties and shock resistance of the resultant polyester resin composition tend to be reduced, and if the
5 logarithmic viscosity is more than 2.0 (dl/g), the molding flowability tends to be reduced since the fusion viscosity is high.

(Silane-treated foliated phyllosilicate)

10 The silane-treated foliated phyllosilicate used in the present invention is a composite in which an organo-silane compound represented by the general formula (1) is introduced in a swellable silicate:

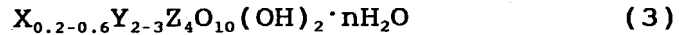


15 (where n is an integer from 0 to 3; Y is a hydrocarbon group with 1 to 25 carbons; the hydrocarbon group may have a substituent(s); X is a hydrolyzable group or hydroxyl group; n Ys may be the same type or different types; and 4-n Xs may be the same type or different types).

20 The above swellable silicate consists of tetrahedral crystalline sheet consisting essentially of silicon oxide, and octahedral crystalline sheet consisting essentially of metal hydroxide. Examples of them include,
25 for example, smectite clay, swellable mica, and the like. Using smectite clay and/or swellable mica as the swellable silicate is preferable because of the dispersibility of the swellable silicate in the resin composition of the present invention and easy obtainability, and in terms of improving
30 the physical properties of the resin composition.

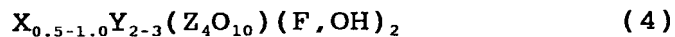
The above smectite clay is represented by the general formula (3) and can be naturally occurring or

synthetic:



(where X is one or more components selected from the group consisting of K, Na, 1/2Ca, and 1/2Mg; Y is one or more
 5 components selected from the group consisting of Mg, Fe, Mn, Ni, Zn, Li, Al, and Cr; and Z is one or more components selected from the group consisting of Si and Al. H₂O represents a water molecule linked to the interlayer ion, and n fluctuates significantly depending on interlayer ion
 10 and relative humidity). Specific examples of the smectite clay include, for example, montmorillonite, beidellite, nontronite, saponite, iron saponite, hectorite, sauconite, stevensite and bentonite, etc., or substituted compounds and derivatives thereof, or mixtures thereof. The basal
 15 spacing of a smectite clay in initial aggregated state is about 10 to 17 Å, and the average grain size of smectite clay in the aggregated state is about 1000 Å to 1000000 Å.

Furthermore, the above swellable mica is
 20 represented by the general formula (4) and can be naturally occurring or synthetic:



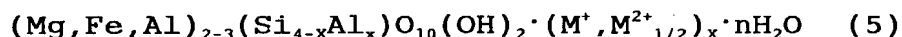
(where X is one or more components selected from the group consisting of Li, Na, K, Rb, Ca, Ba, and Sr; Y is one or
 25 more components selected from the group consisting of Mg, Fe, Ni, Mn, Al, and Li; and Z is one or more components selected from the group consisting of Si, Ge, Al, Fe and B). They have a property of swelling in water, a polar solvent compatible with water in n arbitrary ratio, and a
 30 mixture solvent of water and the polar solvent. For example, they include lithium type taeniolite, sodium type taeniolite, lithium type tetrasilicon mica, and sodium type tetrasilicon mica, or the like, or substituted compounds

or derivatives thereof, or mixtures thereof. The basal spacing of swellable mica in initial aggregated state is about 10 to 17 Å, and the average grain size of swellable mica in an aggregated state is about 1000 Å to 1000000 Å.

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Among the above swellable mica, there are ones having a structure similar to vermiculites, and it is possible to use such vermiculite equivalents. The vermiculite equivalents include 3-octahedron type and 2-octahedron type which are represented by the general formula (5):

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(where M is an exchangeable cation of alkali or alkaline earth metal such as Na and Mg, and $x=0.6$ to 0.9 , $n=3.5$ to 5). The basal spacing of vermiculite equivalents in the initial aggregated state is about 10 to 17 Å, and the average grain size of vermiculite equivalents in the aggregated state is about 1000 Å to 5000000 Å.

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The swellable silicate may be used alone, or may be used in a combination of two or more kinds. Among these, montmorillonite, bentonite, hectorite, and swellable mica having sodium ions at the interlayer, and combinations thereof are preferable because of their dispersibility in the resin compositions of the present invention, and easy obtainability and effects on improving physical properties of the resin composition.

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For the crystal structure of the swellable silicate, a structure with a high purity in which the crystals are regularly laminated along the C-axis direction is desirable. However, a structure in which the crystal cycle is irregular and a plurality of types of crystal structures are mixed

(i.e., mixed-layer mineral) can also be used.

For the organo-silane compounds introduced into the swellable silicate, a commonly used arbitrary organo-silane compound may be used, and the organo-silane compounds represented by the general formula (1):



are typically used. In the general formula (1), n is an integer from 0 to 3; Y is a hydrocarbon group with 1 to 25 carbons; and the hydrocarbon group may have a substituent. Examples of a substituent in the case where the hydrocarbon group having 1 to 25 carbons has a substituent include: a group bonded by ester bond, a group bonded by ether bond; epoxy group, amino group, carboxylic group, a group having a carbonyl group at the terminus, amide group, mercapto group, a group bonded by sulfonyl bond, a group bonded by sulfinyl bond, nitro group, nitroso group, nitrile group, halogen atom, hydroxyl group, and the like. The compound may be substituted with one kind of these, or may be substituted with two or more kinds of these. In the case of hydrocarbon group having a substituent, the total number of carbons including the carbons in the substituent is preferably 1 to 25, but it is not a limitation. X is a hydrolyzable group and/or hydroxyl group. Examples of the hydrolyzable groups include one or more groups selected from the group consisting of alkoxy group, alkenyloxy group, ketoxime group, acyloxy group, amino group, aminooxy group, amide group, and halogen atom. When n or 4-n in the general formula (1) is 2 or more, n Ys and 4-n Xs may be the same kind or different kinds.

In the specification of the present application, the hydrocarbon group means a saturated or unsaturated,

monovalent or polyvalent aliphatic hydrocarbon group with straight chain or branched chain (i.e., having a side chain), aromatic hydrocarbon group or alicyclic hydrocarbon group or aliphatic hydrocarbon group containing aromatic hydrocarbon and/or alicyclic hydrocarbon. Examples of these include alkyl group, alkenyl group, alkynyl group, phenyl group, naphthyl group, cycloalkyl group, and the like. In the specification of the present application, "alkyl group" is intended to include a polyvalent hydrocarbon group such as "alkylene group" unless otherwise noted. Similarly, alkenyl group, alkynyl group, phenyl group, naphthyl group, and cycloalkyl group include alkenylene group, alkynylene group, phenylene group, naphthylene group, and cycloalkylene group, respectively.

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In the general formula (1), examples in the case where Y is a hydrocarbon group having 1 to 25 carbons include: a compound having a straight long chain alkyl group such as decyl trimethoxysilane; a compound having a lower alkyl group such as methyl trimethoxysilane; a compound having an unsaturated hydrocarbon group such as a 2-hexenyl trimethoxysilane; a compound having an alkyl group which has a side chain such as 2-ethylhexyl trimethoxysilane; a compound having a phenyl group such as phenyl triethoxysilane; a compound having a naphthyl group such as 3- β -naphthylpropyl trimethoxysilane, and a compound having an aralkyl group such as p-vinylbenzyl trimethoxysilane. Among the examples in which Y is a hydrocarbon group having 1 to 25 carbons, specific examples of the compounds in which Y is a group having a vinyl group include vinyl trimethoxysilane, vinyl trichlorosilane, and vinyl triacetoxysilane.

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Examples are now listed in which Y has a substituent. Examples of the compound in which Y is a group having a group substituted with a group bonded by an ester group include γ -methacryloxypropyl trimethoxysilane. Examples of the compound in which Y is a group having a group substituted with a group bonded by an ether group include γ -polyoxyethylenepropyl trimethoxysilane and 2-ethoxyethyl trimethoxysilane. Examples of the compound in which Y is a group substituted with an epoxy group include γ -glycidoxypropyl trimethoxysilane. Examples of the compound in which Y is a group substituted with an amino group include γ -aminopropyl trimethoxysilane, γ -(2-aminoethyl)aminopropyl trimethoxysilane, and γ -anilinopropyl trimethoxysilane. Examples of the compound in which Y is a group substituted with a carboxyl group include γ -(4-carboxyphenyl)propyl trimethoxysilane. Examples of the compound in which Y is a group substituted with a group having a carbonyl group in the termini include γ -ureidopropyl triethoxysilane. Examples of the compound in which Y is a group substituted with a mercapto group include γ -mercaptopropyl trimethoxysilane. Examples of the compound in which Y is a group having a group substituted with a group bonded by a sulfonyl group include γ -phenylsulfonylpropyl trimethoxysilane. Examples of the compound in which Y is a group having a group substituted with a group bonded by a sulfinyl group include γ -phenylsulfinylpropyl trimethoxysilane. Examples of the compound in which Y is a group substituted with a nitro group include γ -nitropropyl triethoxysilane. Examples of the compound in which Y is a group substituted with a nitroso group include γ -nitrosopropyl triethoxysilane. Examples of the compound in which Y is a group substituted with a nitrile group include γ -cyanoethyl triethoxysilane and

γ -cyanopropyl triethoxysilane. Examples of the compound in which Y is a group substituted with a halogen atom include γ -chloropropyl triethoxysilane. Other than the above, organo-silane compound in which Y is a group having a hydroxyl group may also be used. Such an example includes N,N-di(2-hydroxyethyl)amino-3-propyl triethoxysilane. The hydroxyl group may be in the form of silanol group (SiOH). Substituted compounds or derivatives of the above organo-silane compounds may also be used. These organo-silane compounds may be used alone or in a combination of two or more kinds.

The basal spacing of the silane-treated foliated phyllosilicate used in the present invention may be in an expanded state compared to the initial basal spacing of the swellable silicate, due to the presence of the introduced organo-silane compound. For example, if an organo-silane compound is not introduced, the swellable silicate which is dispersed in the dispersion medium and the basal spacings thereof have been expanded may return to the state in which the layers of swellable silicate are again aggregated after the dispersion medium is removed. On the other hand, according to the present invention, by introducing an organo-silane compound after the basal spacing is expanded, the obtained silane-treated foliated phyllosilicate can remain in the state in which the basal spacing is expanded without the layers being aggregated after the dispersion medium is removed. The basal spacing of the silane-treated foliated phyllosilicate is 1.3 times or more, preferably 1.5 times or more, more preferably 1.7 times or more, still more preferably 2 times or more, compared to the initial basal spacing of the swellable silicate. Accordingly, by introducing an organo-silane compound and expanding the

basal spacing, it is possible to improve the affinity between the silane-treated foliated phyllosilicate and the resin.

5 Here, it is possible to confirm, by using a variety of methods, that the silane-treated foliated phyllosilicate is formed by the introduction of an organo-silane compound into the swellable silicate. The following method is an example of a confirmation method.

10 First, the silane-treated foliated phyllosilicate is washed with an organic solvent such as tetrahydrofuran or chloroform, whereby organo-silane compound merely adsorbed on the silane-treated foliated phyllosilicate is washed and removed. The washed silane-treated foliated
15 phyllosilicate is grounded in a mortar or the like so as to obtain a powder-like product, and then sufficiently dried. Then, a material for window such as powdered potassium bromide (KBr) are sufficiently mixed with the silane-treated foliated phyllosilicate in a predetermined ratio,
20 and the mixture is pressed to obtain tablets. Then the absorption bands originating from the organo-silane compound are measured by a transmission method or the like, using Fourier transform (FT)-IR. If more accurate measurement is desired or the amount of the introduced
25 organo-silane compound is small, it is desirable to directly measure the sufficiently dried powdered silane-treated foliated phyllosilicate by a diffuse reflectance infrared spectroscopy (DRIFT).

30 It is also possible to confirm, by a variety of methods, that the basal spacing of the silane-treated foliated phyllosilicate is expanded more than the initial basal spacing of the swellable silicate. The following

method is an example of a confirmation method.

Specifically, similar to the above, the silane-treated foliated phyllosilicate is washed with an organic solvent, whereby the organo-silane compound adsorbed on the silane-treated foliated phyllosilicate is removed. After the washed silane-treated foliated phyllosilicate is dried, the expansion may be confirmed by a small-angle X-ray diffraction method (SAXS), or the like. In this method, the value of the X-ray diffraction peak angle originating from (001) plane of the powdered silane-treated foliated phyllosilicate is measured by the SAXS, and the basal spacing can be obtained by applying the measured value to the Bragg's equation for calculation. The initial basal spacing of the swellable silicate is similarly measured, and by comparing these two, the expansion of the basal spacing can be confirmed.

As described above, by FT-IR or the like, the absorption bands originating from the added organo-silane compound after the washing with an organic solvent are observed, and by SAXS it is measured that the resultant basal spacing is expanded more than that of the swellable silicate as the raw material. Accordingly, it is possible to determine that the desired silane-treated foliated phyllosilicate is formed.

(Addition and dispersion of a silane-treated foliated phyllosilicate to a resin composition)

The resin composition according to the present invention is prepared so that the lower limit of the amount of the silane-treated foliated phyllosilicate added to the 100 parts by weight of the resin is typically 0.1 parts by

limit of the ash content ratio in the resin composition originating from the silane-treated foliated phyllosilicate is typically 0.1 % by weight, preferably 0.2 % by weight, more preferably 0.3 % by weight, still more preferably 0.4 % by weight, further preferably 0.5 % by weight, still further preferably 1.0 % by weight, and particularly preferably 1.5 % by weight. The resin composition is prepared so that the upper limit of the ash content ratio is typically 30 % by weight, preferably 28 % by weight, more preferably 25 % by weight, still more preferably 23 % by weight, and particularly preferably 20 % by weight. Herein, the ash content ratio means the percentage by weight of the swellable silicate component which remains after the resin composition is heated to ashes at about 620°C to the resin composition before the heating and ashing. It is measured, for example, based on JIS K 7052.

In the polycarbonate resin composition, if the ash content ratio is less than 0.1 % by weight, the effect of improving mechanical properties, deflection temperature under load, and anisotropy may be insufficient. If the amount is more than 30 % by weight, the exterior appearance and transparency of the molded product tends to be deteriorated. In the polyarylate resin composition, if the ash content ratio is less than 0.1 % by weight, the effect of improving mechanical properties, dimensional accuracy, and a warpage may be insufficient. If the amount is more than 30 % by weight, the transparency and surface smoothness tend to be deteriorated. In the polyester resin composition, if the lower limit of the ash content ratio is less than 0.1 % by weight, the effect of improving moldability and dimensional stability may be insufficient. If the upper

limit of the amount is more than 30 % by weight, the exterior appearance of the molded product and flowability during the molding tend to be deteriorated.

5 The structure of the silane-treated foliated phyllosilicate dispersed in the resin composition according to the present invention is totally different from that of the swellable silicate before the addition, which is an aggregated structure having a size of the order of 1 μ m and
10 with many laminated layers. Specifically, by introducing the organo-silane compound having an affinity with the matrix resin, and by using the silane-treated foliated phyllosilicate having an expanded basal spacing compared to the initial swellable silicate, the layers are exfoliated
15 from each other and fractionated independently from each other. As a result, the silane-treated foliated phyllosilicate is dispersed in the resin composition in very fine thin plate-like shapes which are independent from each other, and the number of which is significantly increased
20 compared to the number of the particles in the swellable silicate as the raw material. The dispersed state of such a thin plate-like silane-treated foliated phyllosilicate in the resin composition can be represented by the following aspect ratio (ratio of layer length to layer thickness),
25 the number of dispersed particles, average layer thickness, and the maximum layer thickness.

 The average aspect ratio of the silane-treated foliated phyllosilicate is defined as the numerical average
30 value of the ratio of the layer length to the layer thickness of the silane-treated foliated phyllosilicate dispersed in the resin. The average aspect ratio of the silane-treated foliated phyllosilicate in the resin composition according

to the present invention is typically 10 to 300, preferably 15-300, and more preferably 20 to 300.

5 In the polycarbonate resin composition, if the
average aspect ratio is less than 10, effect of improving
the modulus of elasticity and deflection temperature under
load may be insufficient. In the polyarylate resin
composition, if the average aspect ratio is less than 10,
10 the effect of improving mechanical properties, dimensional
accuracy, and warpage may be insufficient. In the
polyester resin composition, if the average aspect ratio
is less than 10, the effect of improving the modulus of
elasticity and dimensional stability may be insufficient.
15 Furthermore, in the polyester resin composition, if the
average aspect ratio is less than 10, the numerical values
of $\eta_a - 3\eta$, $\Delta\eta_a$, and $J_{e0} \cdot \eta_0$ described later may not be within
a predetermined range, which results in the tendency of
deteriorating moldability such as the releasability and the
molding cycle. If the average aspect ratio is more than 300,
20 the effect does not change. Therefore, it is not necessary
to increase the average aspect ratio to more than 300.

 The [N] value which represents the number of the
dispersed particles is defined as the number of the dispersed
25 particle in an area of $100 \mu\text{m}^2$ of the resin composition per
unit wt% of the swellable silicate. The [N] value of the
silane-treated foliated phyllosilicate in the resin
composition according to the present invention is typically
30 or more, preferably 45 or more, and more preferably 60
30 or more. Although there is no specific upper limit, the
effect does not change if the [N] value exceeds around 1000.
Therefore, it is not necessary to increase the [N] value
to more than 1000.

The [N] value may be obtained by, e.g., the following method. Specifically, it may be obtained by cutting the resin composition into a super thin segment with a thickness of about 50 μm to 100 μm , and dividing, the number of the particles of the silane-treated foliated phyllosilicate existing in an arbitrary region with an area of 100 μm^2 on the image of the segment taken by a TEM or the like by the weight ratio of the swellable silicate used. Alternatively, the [N] value may be obtained by selecting an arbitrary region on the TEM image in which 100 or more particles exist (the area should be measured in advance), dividing the number of the particles existing in the region by the weight ratio of the swellable silicate used, and then converting the value into the number per an area of 100 μm^2 . Accordingly, the [N] value can be quantified by using a TEM photographing of the resin composition.

The average layer thickness is defined as the numerical average value of the layer thickness of the silane-treated foliated phyllosilicate dispersed in a thin plate-like shape. The upper limit of the average layer thickness of the silane-treated foliated phyllosilicate of the resin composition according to the present invention is 500 Å or less, preferably 450 Å or less, more preferably 400 Å or less. In the polycarbonate resin composition, if the average layer thickness is more than 500 Å, the effect of improving the mechanical properties, deflection temperature under load, and anisotropy may be insufficient. In the polyarylate resin composition, if the average layer thickness is more than 500 Å, the effect of improving mechanical properties, dimensional accuracy, and warpage may be insufficient. In the polyester resin composition,

if the average layer thickness is more than 500 Å, the effect of improving the mechanical properties, heat resistance and dimensional stability may be insufficient. Furthermore, in the polyester resin composition, if the average layer thickness is more than 500 Å, the numerical values of $\eta_s - 3\eta$, $\Delta\eta_s$, and $J_{s0} \cdot \eta_0$ described later may not be within a predetermined range, which results in the tendency of deteriorating the moldability such as releasability and the molding cycle.

Although the lower limit of the average layer thickness is not specifically limited, in the polycarbonate resin composition and the polyarylate composition, it is preferably more than 50 Å, more preferably 60 Å or more, and still more preferably 70 Å or more. On the other hand, in the polyester resin composition, it is more than 10 Å, preferably more than 30 Å, and more preferably more than 50 Å.

The maximum layer thickness is defined as the maximum value of the layer thickness of the silane-treated foliated phyllosilicate dispersed in a thin-plate shape in the resin composition according to the present invention. The upper limit of the maximum layer thickness of the silane-treated foliated phyllosilicate is 2000 Å or less, preferably 1800 Å or less, and more preferably 1500 Å or less. In the polycarbonate resin composition, if the maximum layer thickness is more than 2000 Å, the balance among the mechanical properties, deflection temperature under load, anisotropy, transparency, and surface quality may be deteriorated. In the polyarylate resin composition, if the maximum layer thickness is more than 2000 Å, the balance among the mechanical properties, dimensional

accuracy, warpage, transparency, and surface smoothness may be deteriorated. In the polyester resin composition, if the maximum layer thickness is more than 2000 Å, the surface quality may be deteriorated. Furthermore, in the polyester resin composition, if the maximum layer thickness is more than 2000 Å, the numerical values of η_0 - 3η , $\Delta\eta_0$, and J_{e0} : η_0 described later may not be within a predetermined range, which results in the tendency of deteriorating moldability such as the releasability and the molding cycle.

Although the lower limit of the maximum layer thickness of the silane-treated foliated phyllosilicate is not specifically limited, in the polycarbonate resin composition and the polyarylate resin composition, it is preferably more than 100 Å, more preferably 150 Å or more, and still more preferably 200 Å or more. On the other hand, in the polyester resin composition, it is more than 10 Å, preferably more than 50 Å, and more preferably more than 100 Å.

The layer thickness and the layer length of the silane-treated foliated phyllosilicate can be obtained from the image of a film, thin-walled molded product and the like photographed using a microscope or the like. The film is formed by heat press molding or stretching molding of the resin composition according to the present invention after heating and fusing the resin composition. The thin-walled molded product is obtained by injection molding of a fused resin.

Specifically, a sample piece of a film prepared by the above method, or a thin, flat plate-shaped product molded by an injection molding with a thickness of about 0.5 mm

(Rheology characteristics of the polyester resin composition)

30 The difference ($\eta_e - 3\eta$) between the extensional viscosity η_e and the triple value of the shear viscosity 3η can be an index for the strain hardening property of the resin. The strain hardening property means a property in which the extensional viscosity becomes greater as the

strain becomes greater. Nihon Rheology Gakkaishi, vol. 13, pp. 13 to 23 describes a rate of strain.

5 According to the method for measuring the
extensional viscosity by drawing a sample formed in a rod
shape or a strip shape in a fusion state, if there is no
strain hardening property, the value of the extensional
viscosity increases as the sample is drawn (as the strain
is increased), and then becomes close to 3η , and reaches
10 to a constant value. On the other hand, if there is any
strain hardening property, the value of the extensional
viscosity increases beyond 3η as the strain is increased and
then reaches to a constant value. Specifically, the $\eta_0 - 3\eta$
when there is no strain hardening property is 0 or less
15 while $\eta_0 - 3\eta$ of a resin when there is a strain hardening
property is more than 0, and as the strain hardening property
increases, the value of $\eta_0 - 3\eta$ increases. This is the reason
why the $\eta_0 - 3\eta$ can be the index of a strain hardening property.

20 However, the fusion viscosity of the thermoplastic
polyester resin is low and thus it is impossible to retain
the shape of the sample such as a rod shape or a strip shape
in the molten state. Therefore the above-described method
cannot measure the extensional viscosity. Therefore, the
25 method for measuring the extensional viscosity of the
polyester resin composition according to the present
invention was performed in accordance with the method
described in Japanese Patent Application No. 9-113038.
Specifically, by using a capillary rheometer provided with
30 a longer die and a shorter die having the same diameter,
the pressure loss of fused resin in each of the dies is
measured. The pressure loss in a virtual die with a length
of zero (P_0) is then calculated according to the

equation (6):

$$P_0 = (p_2 \cdot L_1 - p_1 \cdot L_2) / (L_1 - L_2) \quad (6)$$

where p_1 the pressure loss measured in the longer die, p_2 is the pressure loss measured in the shorter die, L_1 is the length of the longer die, and L_2 is the length of the shorter die.

The shear viscosity η and the shear rate $\dot{\gamma}$ can be obtained using a capillary rheometer.

The extensional viscosity η_e and rate of strain $\dot{\epsilon}$ are calculated by the equation (7) and (8), respectively:

$$\eta_e = [9(n+1)^2 p_0^2] / 32 \eta \dot{\gamma}^2 \quad (7)$$

$$\dot{\epsilon} = 4 \eta \dot{\gamma}^2 / 3(n+1) p_0 \quad (8),$$

where $\dot{\gamma}$ is the shear rate and η is the shear viscosity.

n is the power-law index, which is defined by the equation (9):

$$\eta = c \dot{\gamma}^{n-1} \quad (9)$$

where c is a constant.

η_e measured by such a method is the extensional viscosity.

Therefore, it is possible, as described below, to calculate the strain hardening rate from η_e and η obtained by the above-described method. Thus, according to the

present specification, the strain hardening rate refers to the value calculated by the following method.

5 After measuring the extensional viscosity and the shear viscosity of the resin at 280°C by the above-described method, the relationship between the shear rate and the shear viscosity is approximated by the equation (10):

$$\eta = a\dot{\gamma}^p \quad (10),$$

using the least-squares method, thereby obtaining a and p.
10 The relationship between the rate of strain and the extensional viscosity is approximated by the equation (11):

$$\eta = b\dot{\epsilon}^q \quad (11),$$

using the least-squares method, thereby obtaining b and q.

15 The difference ($\eta_e - 3\eta$) between η_e at $\dot{\epsilon} = 100$ (1/s) and 3η at $\dot{\gamma} = 100$ (1/s) is the index of the strain hardening property according to the present invention. Specifically, it can be calculated by

$$b \cdot 100^q - 3a \cdot 100^p.$$

20

Therefore, in the polyester resin composition according to the present invention, the index $\eta_e - 3\eta$ of the strain hardening property at a temperature of 280°C and at a rate of strain of 100 (1/s) is 300 Pa·s or more, preferably 350 Pa·s or more, more preferably 400 Pa·s or more, still more preferably 500 Pa·s or more, and particularly preferably 600 Pa·s or more. If $\eta_e - 3\eta$ is less than 300 Pa·s, the moldability such as the releasability and molding cycle tends to be deteriorated. Although there is no

25

specific upper limit for the index, it is around 15000 Pa·s.

Further, the extensional viscosity can be obtained by the method similar to the above-described method. Therefore, the polyester resin composition according to the present invention has, at a temperature of 280°C, a difference $\Delta\eta_0$ between η_0 at the rate of strain of 100 (1/S) and η_0 at the rate of strain of 1000 (1/S) is 500 Pa·s or more, preferably 600 Pa·s or more, and more preferably 700 Pa·s or more. If $\Delta\eta_0$ is less than 500 Pa·s, the moldability such as the releasability and molding cycle tends to be deteriorated. Although there is no specific upper limit for the extensional viscosity, it is around 15000 Pa·s.

Equilibrium compliance J_{e0} is a measure for the size of elastic deformation and zero shear viscosity η_0 is a measure for the unlikelihood of plastic deformation. Therefore, the product $J_{e0} \cdot \eta_0$ of equilibrium compliance and zero shear viscosity is an index for the maximum relaxation time of resin, which indicates the unlikelihood of an intertwining of polymers to disentangle. Equilibrium compliance J_{e0} and zero shear viscosity η_0 are measured based on the method shown below. First, using a stress controlled type fusion viscoelasticity measurement apparatus, the sample which is sandwiched between a cone and plate is fused, and then a constant stress is applied to the sample for measuring the strain occurred in the sample at 280°C. The creep compliance $J(t)$ at that time is defined by the equation (12):

$$J(t) = \gamma(t) / \sigma \quad (12)$$

wherein $\gamma(t)$ is a strain, σ is a stress, and t is time. $J(t)$

is obtained from the obtained value of the strain, therefrom the creep curve is generated. On one hand, the creep compliance after a sufficient time elapses is indicated in approximation as shown in the equation (13):

$$J(t) = J_{e0} + t/\eta_0 \quad (13)$$

wherein J_{eo} is an equilibrium compliance, and η_0 is a zero shear viscosity. Therefore, according to the equation (13), the approximation of the creep curve is provided as a straight line and from the intercepts of the straight line the equilibrium compliance J_{eo} is calculated, and from the slope of the line η_0 is calculated. The first term (J_{eo}) of the equation (13) represents the size of the elastic deformation, and the second term (t/η_0) represents the size of plastic deformation.

Therefore, $J_{e0} \cdot \eta_0$ of the polyester resin composition of the present invention at a temperature of 280°C is 0.8 seconds or more, preferably 0.9 seconds or more, more preferably 1.0 second or more, still more preferably 1.2 seconds or more, and particularly preferably 1.5 seconds or more. If $J_{e0} \cdot \eta_0$ is less than 0.8 seconds, the moldability such as releasability and molding cycle tends to be deteriorated. Although there is no specific limitation for the upper limit of $J_{e0} \cdot \eta_0$, it is around 20 seconds.

The rheology characteristics of the polyester resin composition of the present invention typically satisfy at least one of the conditions regarding the above-described lower limits for each η_e , 3η , $\Delta\eta_e$ and $J_{e0} \cdot \eta_0$. Preferably at least two of the conditions are satisfied, and more preferably all the conditions are satisfied. In the polyester resin composition, the silane-treated foliated

phyllsilicate exists in a very fine, mutually independent thin-plate shape to a degree which is impossible to achieve by a conventional technique. The number thereof is significantly increased comparing to the number of particles of the raw material of the swellable silicate, whereby a homogeneous micro dispersion is achieved. This state of dispersion provides a significant factor for the rheology characteristics of the polyester resin composition, by which the releasability and molding cycle during fusion molding are improved. During the fusion molding, the dimensional stability (for, example, shrink mark due to crystallization) is not deteriorated. Furthermore, the surface quality of the molded product is not deteriorated since the silane-treated foliated phyllosilicate is dispersed in a very fine thin-plate shape.

(Method for producing a resin composition)

The method for producing the resin composition according to the present invention is not specifically limited, but it is preferably a method which includes the steps of, for example, (A) preparing a clay dispersion including a silane-treated foliated phyllosilicate and a dispersion medium; (B) mixing the clay dispersion and a polymerizable prepolymer which provides a desired resin through polymerization; and (C) polymerizing the polymerizable prepolymer.

Each of the steps (A) to (C) will be now described in detail.

In step (A), the silane-treated foliated phyllosilicate can be prepared by adding an organo-silane compound to a swellable silicate after expanding the basal

spacing of the swellable silicate in the dispersion medium.

The above-described dispersion medium means water, a polar solvent compatible with water, and a mixture solvent of water and a polar solvent compatible with water. The
5 polar solvent includes, for example, alcohols such as methanol, ethanol, isopropanol; glycols such as ethylene glycol, propylene glycol, 1,4-butanediol; ketones such as acetone, methylethylketone; ethers such as diethyl ether, tetrahydrofuran;
10 amide compounds such as N,N-dimethylformamide, N,N-dimethylacetoamide; and other solvents such as pyridine, dimethylsulfoxide, and N-methylpyrrolidone. Diester carbonates such as dimethyl carbonate and diethyl carbonate can also be used as the polar
15 solvent. These polar solvents can be used alone or in combination of two or more kinds.

The expansion of the basal spacing of the swellable silicate in the dispersion medium can be achieved by
20 sufficiently agitating and dispersing the swellable silicate in the dispersion medium. The basal spacing after the expansion is preferably three times the initial basal spacing of the swellable silicate or more, more preferably four times or more, and particularly preferably five times
25 or more. There is no specific upper limit. If the basal spacing expands about 10 times or more, the measurements of the basal spacing will be difficult. In such a case, the swellable silicate exists substantially as a unit layer. Here, the initial basal spacing is referred to the basal
30 spacing of the particle-form swellable silicate before the addition to the dispersion medium, in which the unit layers are laminated with each other to form an aggregated state.

Here, in the specification of the present application, the initial basal spacing of the swellable silicate means the basal spacing of the particle-form swellable silicate before the addition to the dispersion medium, in which the unit layers are laminated with each other to form an aggregated state. The basal spacing can be obtained by a small angle X-ray diffraction method (SAXS), or the like. Specifically, the X-ray diffraction peak angle value of the swellable silicate before the addition to the dispersion medium and the X-ray diffraction peak angle value in the dispersion in which the swellable silicate is dispersed in the dispersion medium are respectively by the SAXS, and then the basal spacing can be calculated and compared by assigning the measured peak angle values to the Bragg's equation.

Examples of methods for efficiently expanding the basal spacing of the swellable silicate include a method of performing the agitation in the dispersion medium at some thousands of rpm or more, and a method of applying an external physical force as described below. The external physical force may be applied using the commonly employed method of wet pulverizing of a filler. A common method of wet pulverizing of a filler includes, for example, a method of using hard particles. In this method, hard particles and the swellable silicate and an arbitrary solvent are mixed and agitated, and by the physical collision between the hard particle and the swellable silicate, the layers of the swellable silicate are separated. The commonly used hard particles are beads for filler grinding and include, for example, glass beads, zirconia beads, or the like. These beads for grinding are selected in consideration of the hardness of the swellable silicate or the materials of the

agitator, and they are not limited to glass or zirconia. The grain size is also determined in consideration of the size of the swellable silicate, and is not absolutely limited by a numerical value. However, it is preferable to use beads
5 having a diameter in the range of 0.1 to 6.0 mm. The solvent used here is not specifically limited, but it is preferable to use the above dispersion media.

As described above, the basal spacing of the
10 swellable silicate is expanded, the layers in the aggregated state are exfoliated and separated, and the layers are made to exist independently. Thereafter, the organo-silane compound is added and agitated. Accordingly, by introducing the organo-silane compound onto the surface of
15 the exfoliated layers of the swellable silicate, the silane-treated foliated phyllosilicate is obtained.

The introduction of the organo-silane compound may be conducted by, in the case of a method using a dispersion
20 medium, adding and agitating the organo-silane compound in the dispersion containing the dispersion medium and the swellable silicate in which the basal spacing is expanded. The method of agitation is not specifically limited, and may be performed using a conventionally known wet agitator.
25 Examples of the wet agitator include a high-speed agitator in which agitating fins rotate at a high speed so as to agitate, a wet mill type in which a sample is wet ground in the gap between the rotor and stator applied with a high shearing speed, a mechanical wet grinder type using a hard
30 medium, a wet collision grinder type in which a sample is collided at a high speed by a jet nozzle or the like, and a wet ultrasonic grinder using ultrasonic wave, etc. If it is desirable to introduce the organo-silane compound more

efficiently, the rotation speed of agitation will be set typically at 500 rpms or more, preferably at 1000 rpms or more, more preferably at 1500 rpms or more, and furthermore preferably at 2000 rpms or more. Alternatively, the shear rate applied will be typically at 300 (1/s) or more, preferably at 500 (1/s) or more, more preferably at 1000 (1/s) or more, and still more preferably at 1500 (1/s) or more. The upper limit of the rotation speed is about 25000 rpms and the upper limit of the shear rate is about 500000 (1/s). An agitation or shearing at these upper limit or more is unlikely to change the effect, and therefore it is not necessary to agitate beyond the upper limit.

In the case of a method using an external physical force, the organo-silane compound can be introduced by adding an organo-silane compound while adding the external physical force to the swellable silicate (e.g., while performing a wet grinding).

Alternatively, the organo-silane compound can also be introduced into the swellable silicate by adding the swellable silicate which has had its basal spacing expanded by the external physical force to a dispersion medium, and then, adding the organo-silane compound to the dispersion medium, in a manner similar to that in the aforementioned method of using a dispersion medium.

The introduction of the organo-silane compound into the swellable silicate can be achieved by the reaction between the hydroxyl group existing on the surface of the swellable silicate with its basal spacing expanded, and the hydrolyzable group and/or the hydroxyl group of the organo-silane compound.

In the case where the organo-silane compound introduced into the swellable silicate further contains a reaction active functional group such as a hydroxyl group, a carboxyl group, an amino group, an epoxy group, or a vinyl group, a compound which may react with such reaction active groups may be further added so as to react the compounds with the reaction active groups. Accordingly, the chain length of the chain of the functional group contained in the organo-silane compound introduced in the swellable silicate can be extended, or the polarity can be changed. In such a case, usable compound to be added may be the aforementioned organo-silane compounds *per se*, but it is not limited to them. An arbitrary compound, for example, a compound containing an epoxy group, a compound containing an amino group, a compound containing a carboxyl group, a compound containing an acid anhydride group, a compound containing a hydroxyl group, and the like can be used depending on the purposes thereof.

The introduction of the organo-silane compound into the swellable silicate and the further reaction with a compound which may react with the reaction active group sufficiently occur at a room temperature, but the system may be heated if necessary. The maximum temperature for heating may be set to any arbitrary temperature so long as it is less than the decomposition temperature of the organo-silane compound used and less than the boiling point of the dispersion medium.

The amount of the organo-silane compound used is adjusted so as to sufficiently enhance the dispersibility of the silane-treated foliated phyllosilicate in the clay

dispersion, affinity between the silane-treated foliated phyllosilicate and the resin, and the dispersibility of the silane-treated foliated phyllosilicate in the resin composition. If necessary, a plurality of kinds of organo-silane compounds having different functional groups from each other can be used together. Therefore, the addition amount of the organo-silane compound is not absolutely limited by a numerical value, but it is typically 0.1 to 200 parts by weight, preferably 0.2 to 180 parts by weight, more preferably 0.3 to 160 parts by weight, still more preferably 0.4 to 140 parts by weight, and particularly preferably 0.5 to 120 parts by weight for 100 parts by weight of the swellable silicate. If the amount of the organo-silane compound is less than 0.1 parts by weight, the micro-dispersion effect of the obtained silane-treated foliated phyllosilicate tends to be insufficient. On the other hand, the addition of 200 parts by weight or more does not change the effects, and therefore it is not necessary to add more than 200 parts by weight.

The method for preparing the clay dispersion is not specifically limited, and it includes, for example, a method of directly using a system which is obtained by preparing the silane-treated foliated phyllosilicate and which contains the dispersion medium and the silane-treated foliated phyllosilicate as the clay dispersion (referred to as the direct method: in this case, Step (A) is the step of preparing silane-treated foliated phyllosilicate); a method of obtaining a system by preparing the silane-treated foliated phyllosilicate, in which the system contains the dispersion medium and the silane-treated foliated phyllosilicate, and adding and mixing another desirable dispersion medium so as to substitute the first dispersion

medium with the newly added dispersion medium, whereby a system consisting of the silane-treated foliated phyllosilicate and the newly added desirable dispersion medium is obtained, which is used as the clay dispersion (referred to as a substitution method); or a method of obtaining silane-treated foliated phyllosilicate by drying and removing a dispersion medium which is sufficiently mixed with a desirable dispersion medium (referred to as the mixing method). In terms of the dispersibility of the silane-treated foliated phyllosilicate, the direct method and the substitution method are preferable, but the mixing method can also be used.

In order to perform the mixing efficiently in the above mixing method, the rotation speed of the agitation is 500 rpm or more, or the shear rate added is 300 (1/s) or more. The upper limit of the rotation speed is 25000 rpm and the upper limit of the shear rate is 500000 (1/s). An agitation beyond these upper limits is not likely to change the effect, and therefore it is not necessary to agitate beyond the upper limit.

In the silane-treated foliated phyllosilicate contained in the clay dispersion obtained in Step (A), the original laminated/aggregated structure the swellable silicate had is substantially completely disappeared, and is fractionated in a thin plate shape or becomes a state in which the spacings between layers expand, i.e., so-called swollen state. As the indicator representing the swollen state, the basal spacing may be used. As described above, in order to make the silane-treated foliated phyllosilicate fractionated and a thin plate shape, the basal spacing of

the silane-treated foliated phyllosilicate in the clay dispersion is preferably three times the initial basal spacing of the swellable silicate or more, more preferably four times or more, and still more preferably five times or more. If the basal spacing is less than three times, the silane-treated foliated phyllosilicate tends not to be efficiently micro-dispersed in the resin composition obtained according to the production method of the present invention.

In order to efficiently expand the basal spacing of the swellable silicate, it is preferable to use water or a mixture solvent of a majority amount of water and a small amount of polar solvent, thereby making a silane-treated foliated phyllosilicate-water dispersion. Herein, a majority amount means the amount in which the volume ratio of water to the dispersion medium is typically 70% or more, preferably 80% or more, and more preferably 90% or more. A small amount means the rest of the majority amount. The water in the water dispersion can be removed during any of the steps in the production process of the resin composition, i.e., Step (A), or the Step (B) or (C) described below. In the case where the polymerization reaction is conducted in a two-phase system, such as an interfacial polymerization, water may be removed after the completion of the polymerization in Step (C). In the case where the polymerization reaction is conducted essentially in a homogeneous system, e.g., in a transesterifying method and in a fusion polymerization method, it is generally easier and helpful for reducing the production time to remove water during Step (B) rather than during Step (A). If water is removed by heat during Step (A), it is necessary to prevent from removing the dispersion medium other than water

simultaneously, which causes the limitation of the temperature, etc., and thus it is inefficient. On the other hand, if water is removed during Step (B), there is no such a limitation and therefore water is efficiently and easily removed.

According to the step (A) described above, a desired clay dispersion can be prepared.

Next, in Step (B), the above-described clay dispersion and a polymerizable prepolymer of a resin can be mixed. Herein, a polymerizable prepolymer means one or more prepolymer selected from polymerizable monomer and oligomer.

In the case of polycarbonate resin, the polymerizable monomer means bisphenols and/or carbonate formable derivatives of bisphenols, and carbonic acid esters described above. In the case of polyarylate resin, the polymerizable monomer means aromatic dicarboxylic acid component (aromatic dicarboxylic acid compound and/or ester formable derivatives of dicarboxylic acid), and diphenol component (diphenol compound and/or ester formable derivatives of diphenol compound) described above. In the case of thermoplastic polyester resin, the polymerizable monomer means dicarboxylic acid compound and/or ester formable derivatives of dicarboxylic acid, and diol compound and/or ester formable derivatives of diol compound.

Oligomer for each of the above resins means a condensate obtained by the reaction of the above-described polymerizable monomer, which has a molecular weight

providing a fusion viscosity enough for the clay dispersion containing the silane-treated foliated phyllosilicate to sufficiently homogeneously disperse in a fusion state. In terms of homogeneous dispersibility of the clay dispersion, the logarithmic viscosity of the oligomer measured at 25°C using a mixture solvent of phenol/tetrachloroethane (5/5 in ratio by weight) is typically less than 0.4 (dl/g), preferably 0.35 (dl/g) or less, and more preferably 0.30 (dl/g) or less. If the logarithmic viscosity is in this range, it is acceptable to add one or two or more other polymerizable monomers to a polyester oligomer in a fused state.

The method for obtaining the above-described oligomer is not specifically limited. For the preparation of oligomer for polycarbonate resin, either of the above interfacial polymerization method, pyridine method, and transesterifying method can be used, but the transesterifying method is preferable. For the preparation of oligomer for polyarylate resin, either of the following interfacial polymerization method and fusion polymerization method (acetate method or phenylester method) can be used, but the interfacial polymerization method is preferable. The preparation of oligomer for thermoplastic polyester resin includes commonly used methods, e.g., a method of esterifying a dicarboxylic acid compound with a diol compound, and a method of transesterifying a diol compound and dicarboxylic acid alkyl ester.

The above-described oligomer can also be obtained by depolymerizing a portion or the whole of a resin with a diol compound. For example, there is a method in which

a portion or the whole of a thermoplastic resin is depolymerized with a diol compound. Specifically, a mixture of a thermoplastic polyester resin and a diol compound as a raw material is heated, and then the temperature is increased to around the temperature range from about 150°C to around the melting point of the thermoplastic polyester resin, so that depolymerization can be effected. Alternatively, the thermoplastic polyester resin as a raw material can be heated in advance to a temperature of the melting point or over, thereby making the thermoplastic polyester resin in the fused state. A diol compound can be then added thereto and agitated, thereby effecting depolymerization. If a copolymerized polyester resin containing residues of a plurality of types of diol compounds is desirable, a diol compound having a structure different from that of the diol component constituting the thermoplastic polyester resin can be added and used for the depolymerization. For the diol compound, one or two or more type(s) of various diol compounds which has been used as the polymerizable monomer for thermoplastic polyester resin can be used. The catalyst necessary for the reaction for obtaining the oligomer for thermoplastic polyester resin is an esterification catalyst, for which one or two or more type(s) of metal oxide, carbonate, acetate, alcholate, and the like can be used. In the depolymerization of the thermoplastic polyester resin, the catalyst necessary for the reaction is usually contained in the starting material thermoplastic polyester resin, but the above esterification catalyst can be further added and used if necessary.

30

The method for mixing the above-described polymerizable prepolymer and the clay dispersion is not specifically limited. For example, the clay dispersion may

be mixed all together with the polymerizable prepolymer which has been made into the fused state or a solution. Alternatively, the method includes a method in which the clay dispersion is added continuously or sequentially over time and mixed. In order to make the polymerizable prepolymer in the fused state or a solution, an extruder or a polymerization reaction machine, for example, may be used. For the addition of the clay dispersion, a liquid adding apparatus may be used. In the case where the clay dispersion is continuously or sequentially added over time, the rate of adding the clay dispersion is not specifically limited, but the clay dispersion is continuously or sequentially added over time at the rate of 0.01 to 10.0 parts by weight per minute, preferably 0.03 to 8.0 parts by weight per minute, and more preferably 0.05 to 6.0 parts by weight per minute for 100 parts by weight of the polymerizable prepolymer.

The timing of the mixing described above is not specifically limited, and the mixing can be performed in an arbitrary stage. For example, in the case of thermoplastic polyester resin, the mixing can be performed in either stages of preparing or storing the polymerizable monomer (in the monomer preparation tank, etc.), conducting a transesterification reaction of the above-described polymerizable monomer (in the transesterification tank), increasing the molecular weight of the transesterified product by condensation polymerization (in the polymerization tank, etc.), after having increased the molecular weight, or the like. The temperature of the system during the mixing is not specifically limited, but in the case of the thermoplastic polyester resin and/or the polymerizable prepolymer of thermoplastic polyester resin

As described above, the polymerizable prepolymer of the resin and the clay dispersion can be mixed according to Step (B).

For the polymerization of polycarbonate resin, an transesterification method is preferably used because of its operability. In the transesterification, for example, a bisphenol compound is added to a mixture containing a carbonic acid diester compound, and sufficiently agitated while heating the system to about 280°C to 300°C, thereby achieving the transesterifying reaction in the fused state. As the catalyst necessary for the transesterification method, one or two or more type(s) of a simple substance, an oxide, a hydroxide, an amide compound, an alcoholate, and a phenolate of an alkali metal or an alkaline-earth metal element, as well as Sb_2O_3 , ZnO , PbO , an organic titanium compound, and quaternary ammonium salt, may be used.

The polymerization in Step (C) is conducted so that the molecular weight of the obtained polycarbonate resin falls within the predetermined range specified above, i.e., the weight average molecular weight Mw measured at 40°C by gel permeation chromatography (GPC) using tetrahydrofuran (THF) solvent is typically 15,000 to 80,000, and preferably 30,000 to 70,000 in terms of monodisperse polystyrene.

For the polymerization of polyarylate resin, an interfacial polymerization method is preferably used. In the interfacial polymerization method, for example, diphenol dissolved in an alkali aqueous solution and aromatic dicarboxylic acid chloride dissolved in an organic solvent such as halogenated hydrocarbon are reacted with each other in the presence of a catalyst at a normal temperature. One or both of the above-described alkali aqueous solution and the organic solvent is the clay dispersion in which the silane-treated foliated phyllosilicate is dispersed. Alternatively, a method may be preferably performed in which clay dispersion is prepared separately, and added and mixed in an arbitrary stage of the reaction between diphenol dissolved in an alkali aqueous solution and aromatic dicarboxylic acid chloride dissolved in an organic solvent such as halogenated hydrocarbon. As the catalyst for the interfacial polymerization, one or two or more type(s) of the catalysts similar to the above-described catalysts for the transesterification method may be used.

In addition to the interfacial polymerization, a fusion polymerization method can also be used for the polymerization of a polyarylate resin. In an acetate method,

which is one of the fusion polymerization methods, diacetylesther of diphenol and aromatic dicarboxylic acid are reacted with each other at a high temperature, whereby a polyarylate resin is obtained. During this
5 polymerization, for example, the clay dispersion can be sequentially added in an arbitrary stage in which the fusion viscosity of the polyarylate resin is at a level of allowing a sufficient homogeneous dispersion of the clay dispersion containing the silane-treated foliated phyllosilicate. In
10 an phenyl ester method, which is another of the fusion polymerization methods, diphenol and diphenyl ester of aromatic dicarboxylic acid are reacted with each other at a high temperature, whereby a polyarylate resin is obtained. During this polymerization, the clay dispersion can be
15 sequentially added at a stage similar to that in the above-described acetate method.

The polymerization in Step (C) is conducted so that the molecular weight of the obtained polyarylate resin falls
20 within the predetermined range specified above, i.e., the weight average molecular weight M_w measured at 25°C by gel permeation chromatography (GPC) using chloroform solvent is typically 15,000 to 80,000, and preferably 30,000 to 70,000 in terms of monodisperse polystyrene.

25 For the polymerization of the thermoplastic polyester resin, for example, a fusion polycondensation method or a solid-phase polymerization method may be used. In the case where a copolymer is obtained using two or more
30 diol compounds, for example, the second diol compound can be added in an arbitrary period during the fusion polycondensation reaction between a dicarboxylic acid and the first diol compound. After the mixing, a further fusion

polycondensation reaction can be conducted. Alternatively, the mixing can be sequentially followed by a solid-phase polymerization. In these polymerization reactions, one or two or more catalysts such as a metal oxide, a carbonate, acetate, and alcoholate may be optionally used.

The polymerization in Step (C) is conducted so that the molecular weight of the obtained thermoplastic polyester resin falls within the predetermined range specified above, i.e., the logarithmic viscosity measured at 25°C using a mixture solvent of phenol/tetrachloroethane (5/5 in ratio by weight) is typically 0.3 to 2.0 (dl/g), preferably 0.35 to 2.0 (dl/g), and more preferably 0.37 to 2.0 (dl/g), and still more preferably 0.40 to 1.8 (dl/g).

As described above, according to Step (C), the polymerizable prepolymer can be converted into a resin having an increased molecular weight in the presence of the clay dispersion.

The polycarbonate resin composition of the present invention has good mechanical properties, a good deflection temperature under load, and a small anisotropy. Moreover, the surface appearance and transparency are not deteriorated, and the relative density is not significantly increased. The polyarylate resin composition of the present invention has a good mechanical property, a good dimensional accuracy, and a small warpage. Moreover, the surface smoothness and transparency are not deteriorated, and the relative density is not significantly increased. Further, the polyester resin composition of the present invention has a good moldability and dimensional stability. Moreover, the exterior appearance of the molded product and

the flowability during molding are not deteriorated. One of the reasons why such desirable characteristic can be obtained is that the silane-treated foliated phyllosilicate is homogeneously dispersed in the resin in the form of numerous tiny thin-plate shape particles. The state of dispersion is represented by either or both of: the average layer thickness (or the average layer thickness and the maximum layer thickness) of the silane-treated foliated phyllosilicate as an indicator, which falls within the range described above; and the number of dispersed particles and the average aspect ratio, which falls within the range described above. For the polyester resin composition according to the present invention, the state of dispersion is further represented by one or more conditions of the rheology characteristics, i.e., $\eta_0-3\eta$, $\Delta\eta_0$ and $J_{e0}\cdot\eta_0$ fall within the range described above.

The state of dispersion of the silane-treated foliated phyllosilicate may be controlled by one or more steps selected from Step (A) and Step (B) in the method of producing the resin composition described above as well as the step of preparing the silane-treated foliated phyllosilicate. The factors to be considered in the control include: in Step (A), the amount of the organo-silane compound, processing conditions (e.g., time, temperature, agitation force, etc.), and if a polar solvent is used, type of the polar solvent, proportion, agitation conditions, and the like; and in Step (B), type and molecular weight of the polymerizable prepolymer, the addition rate of the clay dispersion, and the like.

In the step of preparing the silane-treated foliated phyllosilicate in the dispersion medium (it may be the direct

method in Step (A)), if the agitation force and shear force at dispersing the swellable silicate are constant, the swelling/exfoliating state of the swellable silicate may be changed depending on the type of dispersion medium, and if a plurality of types of dispersion media are used, depending also on the mixing ratio and mixing order of the dispersion media. For example, in the case where montmorillonite is used as the swellable silicate, the montmorillonite is swollen and exfoliated to result in a state approximately close to the unit layer if the dispersion medium is water alone. Therefore, by reacting, while keeping that state, an organo-silane compound which has a group with a high polarity, e.g., an amino group, a mercapto group, or a nitrile group, a clay dispersion can be prepared in which the silane-treated foliated phyllosilicate with substantially the same thickness as that of the unit layer is dispersed. By mixing the above-described clay dispersion with a polymerizable prepolymer in Step (B), the silane-treated foliated phyllosilicate can be formed into the state in which about 5 to about 30 sheets of the unit layers are laminated. On the other hand, in the case where a mixture solvent of water and a polar solvent such as ethanol, tetrahydrofuran (THF), methylethylketone (MEK), pyridine, N,N-dimethylformamide (DMF), N,N-dimethylacetoamide (DMAc), or N-methylpyrrolidone (NMP) is used for the dispersion medium, and in the case where a montmorillonite is dispersed in the polar solvent and then water is added, the montmorillonite is exfoliated and fractionated to result in the state in which several sheets to a hundred and tens of sheets (e.g., about 5 sheets to about 150 sheets, preferably about 10 sheets to about 100 sheets) of unit layers are laminated. By reacting the organo-silane compound in that state, a clay dispersion is prepared in

which the silane-treated foliated phyllosilicate having a thickness approximately corresponding to several sheets to a hundred and tens of sheets (e.g., about 5 sheets to about 150 sheets, preferably about 10 sheets to about 100 sheets) is dispersed. By performing the succeeding steps in the method for producing the resin composition so as to maintain that laminating state, the state of dispersion of the silane-treated foliated phyllosilicate can be controlled.

10 According to the substitution method in Step (A) (the method of substituting the dispersion medium used in preparation of the silane-treated foliated phyllosilicate with another desirable dispersion agent), the state of dispersion of the silane-treated foliated phyllosilicate
15 in the clay dispersion may be changed depending on the type of dispersion medium further added, and if a plurality of types of dispersion media are used, depending also on the mixing ratio and mixing order of the dispersion media. For example, when adding a polar solvent which has a low affinity
20 to the functional group of the organo-silane compound to a dispersion in a water matrix containing a silane-treated foliated phyllosilicate in the state of a unit layer, and then substituting water with the polar solvent, the silane-treated foliated phyllosilicate having been in the
25 state of unit layers aggregates and is laminated in the number of several sheets to tens of sheets (e.g., about 5 sheets to about 50 sheets). By performing the succeeding steps of the method for producing the resin composition so as to maintain that laminating state, the state of dispersion
30 of the silane-treated foliated phyllosilicate can be controlled.

In Step (B), the state of dispersion of the

silane-treated foliated phyllosilicate may be changed depending on the type, molecular weight, and the like of the polymerizable prepolymer mixed with the clay dispersion. By performing the succeeding steps of the method for producing the resin composition so as to maintain that laminating state, the state of dispersion of the silane-treated foliated phyllosilicate can be controlled.

(Formulation and utility of the resin composition)

The resin composition of the present invention comprises polycarbonate resin, polyarylate resin, or thermoplastic polyester resin as the resin component. An arbitrary combination of these resins, e.g., a combination of polycarbonate and polyarylate, a combination of polycarbonate and thermoplastic polyester, and a combination of polyarylate and thermoplastic polyester, may also be preferably used. A shock resistance improving agent can be added, if necessary, to the resin composition of the present invention, such as polybutadiene, butadiene-styrene copolymer, acrylic rubber, ionomer, ethylene-propylene copolymer, ethylene-propylene-diene copolymer, natural rubber, chlorinated butyl rubber, homopolymer of α -olefin, copolymer of two or more types of α -olefin (any copolymer such as random, block, or graft copolymer and a mixture thereof may be included), or a thermoplastic elastomer such as a olefin type elastomer. These agents may be denatured with an acid compound such as maleic anhydride, or an epoxy compound such as glycidyl methacrylate. Furthermore, within a limit which does not deteriorate the properties such as mechanical properties and moldability, one or two or more type(s) of other arbitrary resins may be combined and used, for example, thermoplastic resins such as polyester carbonate resin, liquid crystal polyester

resin, polyolefin resin, styrene type resin (especially, styrene type resin reinforced by a rubber-type polymer), polyamide resin, polyphenylenesulfide resin, polyphenyleneether resin, polyacetal resin, polysulfone resin, polyimide, and polyetherimide, and thermosetting resins such as unsaturated polyester resin, epoxy resin, and phenol novolak resin.

Furthermore, an additive such as a pigment, a dye, a heat stabilizer, an antioxidant, an ultraviolet absorber, a light stabilizer, a lubricant, a plasticizer, a flame resistant agent, and an antistatic agent, may be added to the resin composition of the present invention, depending on the purpose thereof.

Injection molding and heat press molding can be suitably used for producing a molded product from the polycarbonate resin composition of the present invention. The polycarbonate resin composition may be used for blow molding. The resin composition of the present invention may be suitably used for extrusion molding.

The thermoplastic polyester resin composition of the present invention is particularly suitable for materials used for injection molding. As described above, the thermoplastic polyester resin composition is characterized by its rheology characteristics, and specifically, characterized by a difference ($\eta_e - 3\eta$) between an extensional viscosity η_e and the triple value of a shear viscosity η is 300 Pa·s or more; a difference ($\Delta\eta_e$) of values of the extensional viscosity η_e measured at different rates of strain is 500 Pa·s or more; and/or a product $J_{e0} \cdot \eta_0$ of equilibrium compliance J_{e0} and zero shear viscosity η_0

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10

20

limited by these examples.

25

(Materials for polycarbonate resin)

30

* diethyl carbonate: Diethyl carbonate by Wako Pure Chemical Industries, Ltd. (hereinafter, referred to as DEC) was used.

5 * bisphenol A: Bisphenol A by Mitsui Kagaku Co. Ltd. (hereinafter, referred to as BPA) was used.

10 * polycarbonate resin: Tafrone A2200 by Idemitsu Petrochemical Co., Ltd. (hereinafter, referred to as PC resin) was used.

(Materials for polyarylate resin)

15 * isophthaloyl dichloride: Isophthaloyl dichloride by Wako Pure Chemical Industries, Ltd. (Wako standardized) (hereinafter, referred to as IPC) was used.

20 * terephthaloyl dichloride: Terephthaloyl dichloride by Wako Pure Chemical Industries, Ltd. (Wako 1st grade) (hereinafter, referred to as TPC) was used.

25 * bisphenol A: 2,2'-bis(4-hydroxyphenyl)-propane by Wako Pure Chemical Industries, Ltd. (Wako 1st grade) (hereinafter, referred to as bisphenol A) was used.

30 + p-t-butylphenol: P-t-butylphenol by Wako Pure Chemical Industries, Ltd. (Wako 1st grade) (hereinafter, referred to as ptBP) was used. The ptBP was used as a molecular weight controlling agent.

(Materials for thermoplastic polyester resin)

* bishydroxyethyl terephthalate: NISSO-BHET by Nisso Maruzen Chemical K.K. (hereinafter, referred to as BHET) was used.

* dimethyl terephthalate: Wako special grade by Wako Pure Chemical Industries, Ltd. (hereinafter, referred to as DMT) was used.

5

* ethylene glycol: Monoethylene glycol by Nippon Shokubai Kagaku Kogyo Co., Ltd. (hereinafter, referred to as EG) was used.

10 * 1,4-butanediol: 1,4-butanediol by Tosoh Corporation (hereinafter, referred to as 1,4-BD) was used.

* polyethylene terephthalate: PBK2 by Kanebo, Ltd., logarithmic viscosity (η_{inh})=0.63 (dl/g), (hereinafter, referred to as PET) was used.

15

(Materials for silane-treated foliated phyllosilicate)

* swellable silicate:

20 Montmorillonite (trade name: Kunipia F, Kunimine Kogyo K.K., basal spacing: 13 Å) (hereinafter, referred to as natural montmorillonite) was used.

swellable mica (trade name: ME100, Co-op Chemical Co., Ltd., basal spacing: 12 Å) (hereinafter, referred to as swellable mica) was used.

25 bentonite (trade name: Bengel HVP, Houjun Yoko K.K., basal spacing: 13 Å) (hereinafter, referred to as natural bentonite) was used.

30 * γ -(2-aminoethyl)aminopropyl trimethoxysilane: A-1120 by Nippon Unicar Co., Ltd. (hereinafter, referred to as A1120).

* γ -(polyoxyethylene)propyl trimethoxysilane: A-1230 by Nippon Unicar Co., Ltd. (hereinafter, referred to as A1230).

* γ -aminopropyl trimethoxysilane: A-1110 by Nippon Unicar Co., Ltd. (hereinafter, referred to as A1110) was used.

5 * γ -methacryloxypropyl trimethoxysilane: A-174 by Nippon Unicar Co., Ltd. (hereinafter, referred to as A174) was used.

* γ -glycidoxypopyl trimethoxysilane: A-187 by Nippon Unicar Co., Ltd. (hereinafter, referred to as A187)

10

(Other materials)

* glass fiber: T-195H by Nippon Electric Glass Co., Ltd. (hereinafter, referred to as T195H) was used.

15 * tetrahydrofuran: Tetrahydrofuran by Wako Pure Chemical Industries, Ltd. (hereinafter, referred to as THF) was used.

* methylene chloride: Methylene chloride (Wako special grade) by Wako Pure Chemical Industries, Ltd. (hereinafter, referred to as methylene chloride) was used.

20

* polyethylene glycol diglycidyl ether: Polyethylene glycol diglycidyl ether by Sakamoto Yakuhin Kogyo K.K. (trade name: SR8EG) (hereinafter, referred to as PEGDG) was used.

25

* methanol: Methanol Wako Special Grade by Wako Pure Chemical Industries, Ltd. (hereinafter, referred to as MeOH) was used.

30

The evaluation methods in the examples and the comparative examples will be described below.

The average aspect ratio was represented by the numerical average value of the ratio of layer length to layer thickness of each particle of the silane-treated foliated phyllosilicate.

The [N] value was measured as follows. First, the number of the particles of the silane-treated foliated phyllosilicate existing in the selected region was obtained on the TEM image. On the other hand, the ash content ratio of the resin composition originating from the silane-treated foliated phyllosilicate was measured. The above-described number of the particles was then divided by the ash content ratio. The [N] value was represented by the value converted to the value per an area of $100 \mu\text{m}^2$.

The average layer thickness was represented by the numerical average of the layer thickness of each particle of the silane-treated foliated phyllosilicate, and the maximum layer thickness was represented by the maximum value of the layer thickness of each particle of the silane-treated foliated phyllosilicate.

When the dispersed particles were so large that it was inappropriate to observe by TEM, the [N] value was obtained using an optical microscope (Optical microscope BH-2 manufactured by Olympus Optical Co., Ltd.) in a method similar to that described above. The sample was fused, if necessary, at 280 to 320°C using Hot Stage THM600 manufactured by LINKAM, and the state of the dispersed particles was measured in a fused state.

The aspect ratio of the dispersed particles which

were not dispersed in a plate shape was represented by the value of (the major axis)/(the minor axis). Herein, the major axis means, assuming a rectangle having the minimum area among the rectangles circumscribing the image of the subject particle observed by a microscope or the like, the longer side of that rectangle. The minor axis means the shorter side of the rectangle having the minimum area.

(Measurement of the basal spacing by the small angle X-ray diffraction method (SAXS))

The basal spacing were measured, using an X-ray generator (RU-200B manufactured by Rigaku Denki Co., Ltd.) under the measurement conditions of a target CuK α ray, an Ni filter, a voltage of 40 kV, a current of 200 mA, a scanning angle 2θ of 0.2 to 16.0°, and a step angle of 0.02°.

The basal spacing was calculated by applying the small angle X-ray diffraction peak angle value to the Bragg's equation. When confirmation of the small angle X-ray peak angle value was difficult, it was regarded to be difficult because the layers had been sufficiently exfoliated and the crystalline property had substantially disappeared, or because the peak angle value was about 0.8° or less. In that case, the evaluation result of the basal spacing was regarded to be >100 Å.

(Deflection temperature under load)

The polycarbonate resin composition was dried (120°C, 5 hours). The dried resin composition was injection-molded using an injection molding machine (IS-75E manufactured by Toshiba Machine Co., Ltd.) having a clamping force of 75 t, under the conditions of a resin temperature of 300°C, gauge pressure of about 10 MPa, and injection

speed of about 50%, thereby producing a test piece with a size of about 10x100x6 mm. The deflection temperature under load of the obtained test piece (referred to as HDT in the tables below) was measured in accordance with
5 ASTM D-648.

For the polyester resin composition, the measurement was conducted similarly to the above, except that the drying temperature was set at 140°C and the resin
10 temperature during the injection molding was set at 250°C to 280°C.

(Flexural property)

The polycarbonate resin composition was dried
15 (120°C, 5 hours). The dried resin composition was injection-molded using an injection molding machine (IS-75E manufactured by Toshiba Machine Co., Ltd.) having a clamping force of 75 t, under the conditions of a resin temperature of 300°C, gauge pressure of about 10 MPa, and injection
20 speed of about 50%, thereby producing a test piece with a size of about 10x100x6 mm. The flexural strength and flexural modulus of the obtained test piece were measured in accordance with ASTM D-790.

25 For the polyarylate resin composition, the measurement was conducted similarly to the above, except that the resin temperature during the injection molding was set at 320°C.

30 For the polyester resin composition, the measurement was conducted similarly to the above, except that the drying temperature was set at 140°C and the resin temperature during the injection molding was set at 250°C

to 280°C.

(Dimensional accuracy; anisotropy)

5 For the polycarbonate resin composition and the
polyarylate resin composition, anisotropy was evaluated as
the ratio of coefficient of linear expansion between MD
direction and TD direction, using JIS No.1 dumbbell-shaped
test pieces with a thickness of about 3 mm produced under
the conditions similar to those in the flexural property
10 evaluation described above. As the ratio is the closer to
1, anisotropy becomes the smaller and the resin composition
is more isotropic, i.e., the dimensional accuracy becomes
better. The coefficient of linear expansion was measured
as follows.

15 About 7 mm × 7 mm of the center portion of the
above-described dumbbell-shaped test piece was cut out.
The test piece was kept at 20°C for 5 minutes using SSC-
5200 and TMA-120C manufactured by Seiko Denshi K.K., and
20 then the temperature was increased from 20°C to 150°C at a
rate of 5°C/min. The coefficient of linear expansion was
calculated within the range of 30 to 120°C.

(warpage)

25 The polycarbonate resin composition was dried
(120°C, 5 hours), and then injection-molded using an
injection molding machine (IS-75E manufactured by Toshiba
Machine Co., Ltd.) having a clamping force of 75 t under
the conditions of a mold temperature of 80°C, resin
30 temperature of 300°C, gauge pressure of about 10 MPa, and
injection speed of about 50%, thereby producing a flat
plate-like test piece with a size of about 120×120×1 mm. The
above-described flat plate-like test piece was put on a flat

(Surface appearance/surface smoothness)

For the polycarbonate resin composition, the polyarylate resin composition, and polyester resin composition, surface appearance, i.e., surface smoothness, was evaluated as the center line average roughness using JIS No.1 dumbbell-shaped test pieces with a thickness of about 3 mm produced under the conditions similar to those in the dimensional accuracy evaluation.

The center line average roughness was measured using a surface roughness meter, Surfcom 1500A, manufactured by Tokyo Seimitsu Co., Ltd.

(GPC)

About 4 mg of the polyarylate resin composition was dissolved in about 6 g of chloroform. After filtering with a 0.5 μ m filter (made of PTFE), the measurement was conducted using GPC manufactured by WATERS under the conditions of a column temperature of 40°C, chloroform for the carrier solvent, a flow rate of 1 mL/min, and an injection amount of 10 μ L, whereby the weight average molecular weight (Mw) in polystyrene conversion was calculated.

(Ash content ratio)

For the polycarbonate resin composition, the polyarylate resin composition, and polyester resin composition, the ash content ratio originating from the silane-treated foliated phyllosilicate was measured according as JIS K7052.

(Production time)

For the polyester resin composition, the start of the production was defined as the time when the preparation of the silane-treated foliated phyllosilicate-water

dispersion was started at Step (A). The completion of the production was defined as the time when the logarithmic viscosity reached to 0.60 in the PET system, and to 0.80 in the PBT system. The required time was measured and regarded as the production time.

(Logarithmic viscosity)

After drying the obtained polyester resin composition (140°C, four hours), about 100 mg of the dried polyester resin composition was precisely measured and 20 ml of a mixture solvent of a phenol/1,1,2,2-tetrachloroethane (ratio by weight:1/1) was added thereto and dissolved at 120°C. The viscosity of the solution was measured using an Ubbelohde viscometer and an automation viscosity measuring apparatus (Viscotimer manufactured by Lauda), and at a measurement temperature of 25°C for the PET system and a measurement temperature of 20°C for the PBT system. The logarithmic viscosity (η_{inh}) was obtained from the following equation:

$$20 \quad \eta_{inh} = \{ \ln(t/t_0) \} / C$$

where t is the value of the solution, t_0 is the value of the mixture solvent alone, and C is the concentration (g/dl).

The logarithmic viscosity of oligomer was measured
25 in a similar manner to the above.

(Equilibrium compliance J_{e0} and zero shear viscosity η_0)

The polyester resin composition was molded by thermopressing under the conditions of a temperature of 280°C, and a pressure of $4.9 \times 10^6 \text{ N/m}^2$, thereby obtaining a sheet with a thickness of 1.4 mm. A disc having a diameter of 25 mm was cut out from the obtained sheet and served as the sample for measurement.

10

15

The creep curve of the creep compliance $J(t)$ was then approximated by a straight line as in the equation (13):

From the intercept of the straight line, the equilibrium compliance J_{e0} was calculated, and from the gradient of the straight line, the zero shear viscosity η_0 was calculated.

25

Using a twin capillary rheometer configured by arranging two capillary rheometers (manufactured by Rosand Precision), a die having an $L_1=16$ mm and $D_1=1$ mm (referred to as a long die) and a die having an $L_2=0.25$ mm and $D_2=1$ mm (referred to as a short die) are attached, respectively, to each of the capillary rheometers. The barrels and the dies are set at 280°C and the same amount of the polyester resin composition was supplied to each of them and fused. The fused polyester resin composition was then extruded

simultaneously, and the values of the pressure loss p_1 and p_2 were measured at a shear rate within the range of 20 to 200 (1/s). From the obtained values of the pressure loss, the pressure loss p_0 of a virtual die with a length of 0 was calculated using the equation (6):

$$p_0 = (p_2 \cdot L_1 - p_1 \cdot L_2) / (L_1 - L_2) \quad (6)$$

where p_1 is the pressure loss measured with the long die, p_2 is a pressure loss measured with the short die, L_1 is the length of the long die, and L_2 is the length of the short die.

The extensional viscosity η_e and rate of strain $\dot{\epsilon}$ are calculated by the equation (7) and (8), respectively:

$$\eta_e = [9(n+1)^2 p_0^2] / 32 \eta \dot{\gamma}^2 \quad (7)$$

$$\dot{\epsilon} = 4 \eta \dot{\gamma}^2 / 3(n+1) p_0 \quad (8),$$

where $\dot{\gamma}$ is the shear rate and η is the shear viscosity. n is the power-law index, which is defined by the equation (9):

$$\eta = c \dot{\gamma}^{n-1} \quad (9)$$

where c is a constant.

The relationship between the shear rate and the shear viscosity is approximated by the equation (10):

$$\eta = a \dot{\gamma}^p \quad (10),$$

using the least-squares method, thereby obtaining a and p . The relationship between the rate of strain and the extensional viscosity was approximated by the equation (11):

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$$\eta_e = b \dot{\epsilon}^q \quad (11),$$

using the least-squares method, thereby calculating b and q .

5 The difference ($\eta_e - 3\eta$) between η_e at $\dot{\epsilon} = 100$ (1/s) and 3η at $\dot{\gamma} = 100$ (1/s) is the index of the strain hardening property according to the present invention. Specifically, it was calculated by

$$b \cdot 100^q - 3a \cdot 100^p.$$

10

(Releasability)

15 The polyester resin composition of the present invention was dried (140°C, 5 hours), and then injection-molded using an injection molding machine (IS-75E manufactured by Toshiba Machine Co., Ltd.) having a clamping force of 75 t, under the conditions of a resin temperature of 250 to 280°C, gauge pressure of about 10 MPa, injection speed of about 50%, and the cooling time after resin filling of 20 seconds, thereby obtaining a flat plate-shaped test
20 piece with a size of about 120×120×1 mm.

 The die temperature is set at 60, 80, 100, or 120°C, and the releasability at respective temperature was evaluated by classifying into three ranks according to the following legend:

25 ○: released without any difficulty by ejector pins;
 △: unable to release by ejector pins, so that it was released by hand, thereby obtaining a flat plate-shaped sample piece; and
 ×: unable to release by ejector pins, so that it was released
30 by hand, causing the sample piece to be significantly

deformed.

(Cooling time)

As the index for the duration of the molding cycle, the cooling time after the resin was filled into the mold by injection molding was used. A shorter cooling time is preferable since it achieves a shorter duration of the molding cycle.

The cooling time was evaluated as follows. First, the polyester resin composition, which had been dried at 140°C for five hours, was injection-molded using an injection molding machine (IS-75E manufactured by Toshiba Machine Co., Ltd.) having a clamping force of 75 t, under the conditions of a resin temperature of 250 to 280°C, gauge pressure of about 10 MPa, and injection speed of about 50%, thereby obtaining a test piece with a size of about 10x100x6 mm. The cooling time which was required during the molding in order to prevent a deformation, was measured. The mold temperature was set at 60, 80, 100, or 120°C.

In the following examples, the advantages of the polycarbonate resin composition according to the present invention will be described in comparison with comparative examples.

(Example 1-1)

Step (A)

In 7000 g of ion exchanged water, 125 g of natural montmorillonite was added and mixed by agitation for 5 minutes at 5000 rpm using a wet mill by Nippon Seiki K.K. Added thereto was 14 g of Al120, and by further agitation under the conditions shown in Table 1-1, the silane-treated

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foliated phyllosilicate was prepared. The confirmation of silane-treated foliated phyllosilicate was performed by measuring the basal spacing of the separated, dried, and ground solid component by SAXS, and by measuring the absorption bands of functional groups originating from the organo-silane compound in the sample washed with THF, by FT-IR. The results of this are shown in Table 1-1 (the results of Examples 1-2 to 1-6 are also shown in Table 1-1). 1000 g of DEC was then added, and after sufficient mixing, the water was removed by heating, i.e., by a substitution method, whereby the clay dispersion containing the silane-treated foliated phyllosilicate and DEC (referred to as ASi-Mol/DEC) was prepared. The basal spacing of the silane-treated foliated phyllosilicate in the clay dispersion was $>100 \text{ \AA}$.

Step (B)

2240 g of BPA and 2000 g of DMC, and 20 g of dibutyl tin oxide were provided in an autoclave, and by reacting them by bubbling with a dry nitrogen gas at a temperature of 160°C and a pressure of 7 kg/cm^2 (68.6 MPa), bismethylcarbonic acid ester of BPA (referred to as the polymerizable prepolymer a) was prepared. The temperature was kept at 230°C to 240°C , to which the clay dispersion ASi-Mol/DEC prepared in Step (A) was sequentially added and mixed while strongly agitating at 180 rpm. The addition rate of the clay dispersion is about 1300 g/hour.

Step (C)

Then, by subjecting the resultant mixture to fusion polycondensation at a reaction temperature of 230°C to 240°C and at 1 torr (0.133 MPa) or less, a polycarbonate resin

composition containing the silane-treated foliated phyllosilicate was obtained, which was then evaluated. The ash content ratio and the properties are shown in Table 1-2 (the results of Examples 1-2 to 1-6 are also shown in Table 1-2).

(Example 1-2)

Example 1-2 was conducted similarly to Example 1, except that in Step (A) the amount of A1120 was set at 8 g and the clay dispersion (ASi-Mo2/DEC) was prepared by a substitution method. A polycarbonate resin composition containing the silane-treated foliated phyllosilicate was obtained, which was then evaluated.

(Example 1-3)

Example 1-3 was conducted similarly to Example 1, except that in Step (A), 22 g of A1230 (hydrolyzed at pH 3.0 in advance) instead of 14 g of A1120 was used and the clay dispersion (ESi-Mo/DEC) was prepared by a substitution method (and the addition rate of the clay dispersion was about 1000 g/hour). A polycarbonate resin composition containing the silane-treated foliated phyllosilicate was obtained, which was then evaluated.

(Example 1-4)

In Step (A), a swellable mica was used instead of montmorillonite and the amount of A1120 was changed to 28 g to prepare the clay dispersion (ASi-Mi/DEC) by a substitution method (in this case, the basal spacing of the silane-treated foliated phyllosilicate in the clay dispersion was 65 Å). Other than that, Example 1-4 was conducted similarly to Example 1 (however, the addition rate of the clay dispersion was about 800 g/hour). A

polycarbonate resin composition containing the silane-treated foliated phyllosilicate was obtained, which was then evaluated.

5 (Example 1-5)

Step (A)

Asi-Mol/DEC was prepared similarly to Example 1 by a substitution method.

10 Step (B)

BPA (2240 g), which is a reactive monomer of the polycarbonate resin, the above clay dispersion ASi-Mol/DEC and 20 g of dibutyl tin oxide are provided in an autoclave, and then mixed by bubbling with dry nitrogen gas at a
15 temperature of 160°C and at a pressure of 7 kg/cm² (68.6 MPa), whereby the mixture was reacted so as to prepare bisethylcarbonic acid ester of BPA containing the silane-treated foliated phyllosilicate.

20 Step (C)

Then, by conducting fusion polycondensation at a reaction temperature of 230°C to 240°C and under reduced pressure of 1 torr (0.133 MPa) or less, a polycarbonate resin composition containing the silane-treated foliated
25 phyllosilicate was obtained, which was then evaluated.

(Example 1-6)

Step (A)

In 3500 g of ion exchanged water, 160 g of Kunipia
30 F was added and mixed by agitation for 5 minutes at 5000 rpm using a wet mill by Nippon Seiki K.K. Then, 30 g of Al230 was added, and by further agitation under the conditions shown in Table 1-1, the silane-treated foliated

phyllosilicate-water dispersion containing the silane-treated foliated phyllosilicate and water was prepared (The confirmation of the silane-treated foliated phyllosilicate was performed by measuring the basal spacing of the separated, dried, and ground solid component by SAXS, and by measuring the absorption bands of functional groups originating from the organo-silane compound in the sample washed with THF by FT-IR). The results of this are shown in Table 1-1.

10 Step (B)

2240 g of BPA and 2620 g of DEC, and 20 g of dibutyl tin oxide were provided in an autoclave, and they were sufficiently mixed at a temperature of about 115°C. The temperature was kept at about 115°C and the silane-treated foliated phyllosilicate-water dispersion prepared in Step (A) was then sequentially added and mixed while strongly agitating at about 180 rpm. The addition rate of the clay dispersion was about 1000 g/hour. After the addition, the agitation was continued another about 4 hours so as to evaporate and remove water.

Step (C)

By conducting a reaction at a temperature of 160°C and a pressure of 7 kg/cm² (68.6 MPa), and then subjecting to fusion polycondensation at a reaction temperature of 230°C to 240°C and at 1 torr (0.133 MPa) or less, a polycarbonate resin composition containing the silane-treated foliated phyllosilicate was obtained, which was then evaluated.

30

(Comparative Example 1-1)

The polycarbonate resin was obtained by a method similar to that in Example 1-1, but without using a clay

dispersion. The resultant resin was then evaluated. The results are shown in Table 1-3 (The results of Comparative examples 1-2 to 1-5 are also shown in Table 1-3)

5 (Comparative Example 1-2)

The polycarbonate resin composition was obtained by a method similar to that in Example 1, except that 125 g of natural montmorillonite was used instead of the clay dispersion ASi-Mol/DEC. The resultant resin composition
10 was then evaluated.

(Comparative example 1-3)

14 g of A1120 was directly sprayed on 125 g of natural montmorillonite using a sprayer, and then by mixing
15 for an hour, the montmorillonite was treated with silane. The basal spacing of the silane-treated natural montmorillonite was 13 Å. This montmorillonite was washed with THF and then subjected to FT-IR measurement. As a
20 result, the absorption bands originating from primary amino group, secondary amino group, and methylene group were observed.

A polycarbonate resin composition was obtained by a method similar to that in Example 1, except that the
25 above-described silane-treated natural montmorillonite was used instead of the clay dispersion ASi-Mol/DEC. The resultant polycarbonate resin composition was then evaluated.

30 (Comparative Example 1-4)

125 g of montmorillonite and 1000 g of DEC were agitated and mixed for 5 minutes at 5000 rpm using a wet mill, so that a mixture liquid was obtained.

A polycarbonate resin composition was obtained by a method similar to that in Example 1, except that the above mixture liquid was used instead of the clay dispersion ASi-Mol/DEC. The resultant polycarbonate resin composition was then evaluated.

(Comparative Example 1-5)

2500 g of PC resin and 250 g of T195H were subjected to fusion kneading using a biaxial extruder (The Nippon Steel Works, Ltd., LABOTEX 30, at a set temperature of 270 to 290°C and the number of rotations of 100 rpm), and a resin composition was obtained. The resultant resin composition was then evaluated.

(Table 1-1)

Examples		1-1	1-2	1-3	1-4	1-5	1-6
Ion exchanged water	g	7000	7000	7000	7000	7000	3500
Natural montmorillonite		125	125	125		125	160
Swellable mica					125		
A1120		14	8		28	14	
A1230				22			30
Agitation condition: rotation	rpm	5000	5000	5000	6000	5000	5000
Agitation condition: time	hr	1.5	1.5	2.5	3.0	1.5	1.5
Basal spacing of isolated clay composite	Å	26	23	22	17	26	23
Functional group measured by FT-IR		primary amino group, secondary amino group, methylene group	primary amino group, secondary amino group, methylene group	ether group, methylene group	primary amino group, secondary amino group, methylene group	primary amino group, secondary amino group, methylene group	ether group, methylene group

(Table 1-2)

Examples		1-1	1-2	1-3	1-4	1-5	1-6
Step (A)	Ion exchanged water	7000	7000	7000	7000	7000	3500
	Natural montmorillonite	125	125	125	125	125	160
	Swellable mica	14	8	22	28	14	30
	A1120	1000	1000	1000	1000	1000	
	A1230	1000	1000	1000	1000	1000	
Step (B)	DEC	ASI-Mo1 /DEC	ASI-Mo2 /DEC	ESI-Mo /DEC	ASI-Mi /DEC	ASI-Mo1 /DEC	ESI-Mo1 /water
	Clay dispersion	>100	>100	>100	65	>100	>100
	basal spacing of the silane-treated foliated phyllosilicate(Å)						
	a(*1)	○	○	○	○	○	○
	b(*2)						
Step(C)	Polymerizable prepolymer						
	c(*3)						
	Method of mixing the prepolymer and clay dispersion	○	○	○	○	○	○
	mixing by sequential addition(*4)						
	mixing by single addition(*5)						
Step(C)	Addition rate of the clay dispersion	g/hour					
		1300	1300	1000	800	—	1000
fusion polycondensation		4.8	4.8	4.8	4.9	4.8	4.9
Step(C)	Ash content ratio	wt%					
	Average layer thickness	Å	131	204	258	388	145
	Maximum layer thickness	Å	438	625	775	1563	450
	Number of dispersed particles	/wt%·100 μ ²	103	74	70	38	98
	Aspect ratio		152	98	78	48	138
Step(C)	Flexural strength	MPa	139	131	131	125	138
	Flexural modulus	MPa	4080	3650	3610	3310	4010
	HDT	°C	148	144	143	141	146
	Coefficient of linear expansion	/°C × 10 ⁻⁵	5.32	5.64	5.88	6.02	5.34
			5.33	5.66	5.91	6.06	5.35
Step(C)	Anisotropy		0.998	0.996	0.995	0.993	0.998
	Warpage		small	small	small	small	small
	Transparency(Haze)	%	4.3	4.5	5.2	7.8	4.4
	Surface appearance (center line roughness)	μm	0.04	0.04	0.06	0.06	0.04

Comparative Examples			1-1	1-2	1-3	1-4	1-5
Natural montmorillonite		g		125	125	125	250
Silane-treated montmorillonite							
Glass fiber							
DEC					1000		
PC resin						2500	
Polymerizable prepolymer a (*1)			○	○	○	○	—
Ash content ratio		wt%	0	4.9	4.8	4.8	4.8
Average layer thickness (*2)		Å	Not measured	32,000	35,000	3600	Not measured
Maximum layer thickness (*3)		Å	Not measured	900,000	900,000	8800	Not measured
Number of dispersed particles		/wt%·100μ ²	Not measured	1	1	3	Not measured
Aspect ratio (*4)			Not measured	1.5	1.5	1.6	Not measured
Flexural strength		MPa	95	97	97	99	99
Flexural modulus		MPa	2400	2470	2480	2620	4020
HDT		°C	134	135	135	135	158
Coefficient of linear expansion	MD	／°C·10 ⁻⁵	7.41	7.39	7.42	7.05	1.51
	TD	／°C·10 ⁻⁵	7.42	7.40	7.43	7.08	15.06
Anisotropy	MD/TD		0.999	0.999	0.999	0.996	0.100
Warpage			small	medium	medium	medium	large
Transparency(Haze)		%	2.1	32.1	35.2	28.9	45.2
Surface appearance (center line roughness)		μ m	0.020	0.806	0.812	0.668	1.506

5

(*2) This is represented by the numeral average value of the length of the minor axis of the dispersed particle, since it was not dispersed in a plate shape.

(*4) This is represented by ratio of (the length of the major
5 axis)/(the length of the minor axis) of the dispersed
particle, since it was not dispersed in a plate shape.

(Example 2-1)
Step (A)

30 30 g of PEGDG was then added, and after another 30 minutes continuous agitation, the sample was dried and powder was obtained. The sample was washed with THF after drying and powdering, and FT-IR measurement was performed, thereby the absorption bands of functional groups

originating from ether bond were confirmed.

As the dispersion medium, methylene chloride was used. The above silane-treated foliated phyllosilicate and 14000 mL of methylene chloride were sufficiently mixed by a high-speed agitator (5000 rpm x 30 minutes), whereby a clay dispersion containing the silane-treated foliated phyllosilicate and methylene chloride was prepared. The basal spacing of the silane-treated foliated phyllosilicate in the clay dispersion was >100 Å.

Step (B)

Under a nitrogen atmosphere, 945 g of IPC and 235 g of TPC were dissolved in the above clay dispersion and agitated, thereby obtaining a mixture containing the clay dispersion and an aromatic dicarboxylic acid compound. The mixture was cooled to 5°C.

Step (C)

Under a nitrogen atmosphere, 1280 g of bisphenol A, 41 g of ptBP, 10 g of sodium hyposulfite, and 2870 mL of 5N sodium hydroxide aqueous solution were added in 14000 mL of ion exchanged water and sufficiently mixed, and then the resultant product was cooled to 5 °C, whereby an alkali aqueous solution of a phenol compound was prepared.

Then, under a nitrogen atmosphere, 4000 ml of ion exchanged water and 19 g of benzyltriethylammonium chloride, which is an phase transfer catalyst, were charged in another reaction container which had been separately prepared and cooled to 5°C.

This cooled aqueous solution containing the phase

transfer catalyst was agitated at 500 to 800 rpm, into which the above alkali aqueous solution of bisphenol A which had been prepared in advance and the mixture containing the clay dispersion and the aromatic dicarboxylic acid compound, which had been prepared in Step (B), were simultaneously and continuously added together while mixing over about 30 minutes, and then it was agitated for 3 hours. After that, by neutralization, removal of the salts by water washing, and drying, a polyarylate resin composition was obtained, which was evaluated. The results are shown in Table 2-2 (The results of Examples 2-2 to 2-5 are also shown in Table 2-2).

(Example 2-2)

Step (A)

A clay dispersion was prepared similarly to Example 2-1, except that the amount of A1110 was set at 15 g and the amount of PEGDG was set at 15 g. The results are shown in Table 2-1. The basal spacing of the silane-treated foliated phyllosilicate in the clay dispersion was 75 Å.

Steps (B), (C)

Steps (B) and (C) were conducted similarly to Example 1, whereby a polyarylate resin composition was obtained and evaluated.

(Example 2-3)

Step (A)

The clay dispersion was prepared similarly to Example 2-1, except that the amount of A1110 was set at 20 g, and 20 g of A1230 (hydrolyzed at pH 3.0 in advance) was used instead of PEGDG. The results are shown in Table 2-1. The basal spacing of the silane-treated foliated phyllosilicate

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in the clay dispersion was 69 Å.

Steps (B), (C)

5 Steps (B) and (C) were conducted similarly to Example 2-1, whereby a polyarylate resin composition was obtained and evaluated.

(Example 2-4)

Step (A)

10 A clay dispersion was prepared similarly to Example 2-1, except that 180 g of natural bentonite was used instead of natural montmorillonite. The results are shown in Table 2-1. The basal spacing of the silane-treated foliated phyllosilicate in the clay dispersion was >100 Å.

15

Steps (B), (C)

Steps (B) and (C) were conducted similarly to Example 2-1, whereby a polyarylate resin composition was obtained and evaluated.

20

(Example 2-5)

Step (A)

25 3500 g of ion exchanged water and 160 g of natural montmorillonite were mixed by agitation for 5 minutes at 5000 rpm using a wet mill by Nippon Seiki K.K. 45 g of A1230 was then added, and by further agitation under the conditions shown in Table 2-1, the silane-treated foliated phyllosilicate-water dispersion containing the silane-treated foliated phyllosilicate and water was prepared.

30 The prepared silane-treated foliated phyllosilicate-water dispersion was transferred into a first container for addition.

In a second container for addition, under a nitrogen atmosphere, 14000 mL of methylene chloride, 945 g of IPC, and 235 g of TPC were charged and then dissolved and mixed, whereby a methylene chloride solution of aromatic dicarbonic acid was prepared and cooled to 5°C.

In a third container for addition, under a nitrogen atmosphere, 1280 g of bisphenol A, 41 g of ptBP, 10 g of sodium hyposulfite, and 2870 mL of 5N sodium hydroxide aqueous solution were added in 14000 mL of ion exchanged water and sufficiently mixed, and then the resultant product was cooled to 5 °C, whereby an alkali aqueous solution of a phenol compound was prepared.

Step (C)

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After the above dropping, the sample was kept agitated for 3 hours so as to continue polymerization. After that, by neutralization, removal of the salts by water washing, and drying, a polyarylate resin composition was obtained, which was then evaluated.

(Comparative Example 2-1)

The polyarylate resin was obtained by a method similar to that in Example 2-5, and then evaluated. The results are shown in Table 2-3. (The results of Comparative Examples 2-2 to 2-5 are also shown in Table 2-3)

(Comparative Example 2-2)

160 g of natural montmorillonite and 14000 mL of methylene chloride were agitated and mixed for 30 minutes at 5000 rpm by a high-speed agitator. The polyarylate resin was polymerized similarly to Example 2-1, except that the above mixture was used instead of the clay dispersion.

(Comparative Example 2-3)

By directly mixing 160 g of natural montmorillonite, 30 g of A1110, and 30 g of PEGDG at a room temperature for an hour, the natural montmorillonite was treated. The basal spacing of the silane-treated montmorillonite was 13 Å. The silane-treated montmorillonite and 14000 mL of methylene chloride were agitated and mixed for 30 minutes at 5000 rpm by a high-speed agitator. The polyarylate resin was polymerized similarly to Example 2-1, except that the above mixture was used instead of the clay dispersion.

(Comparative Example 2-4)

768 g of ion exchanged water and 256 g of natural montmorillonite were mixed while applying ultrasonic wave,

whereby the natural montmorillonite was swelled.

3700 g of a polyarylate resin polymerized in a method similar to that in Example 2-5 and the above mixture were fused and kneaded under a condition with a temperature of 300 to 320°C and the number of rotations of 350 rpm, using a biaxial extruder (The Nippon Steel Works, Ltd., TEX 44). Volatile moisture was removed through a vent hole under reduced pressure.

(Comparative Example 2-5)

2200 g of a polyarylate resin polymerized in a method similar to that in Example 2-5 and 240 g of glass fiber T195H were fused and kneaded under the same condition as in Comparative Example 2-4.

Examples		2-1	2-2	2-3	2-4	2-5
Ion exchanged water	g	3500	3500	3500	3500	3500
Natural montmorillonite	g	160	160	160		160
Natural bentonite	g				180	
A1110	g	30	15	20	30	
A1230	g			20		45
Agitation rotation	rpm	5000	5000	5000	5000	5000
Agitation time	min.	60	60	90	60	90
Basal spacing of the isolated clay composite	Å	25	22	20	25	22
Functional group measured by FT-IR		primary amino group, methylene group	primary amino group, methylene group	primary amino group, methylene group, ether group	primary amino group, methylene group	methylene group, ether group
PEGDG	g	30	15	0	30	0
Agitation rotation	rpm	5000	5000	—	5000	—
Agitation time	min.	30	30	—	30	—

(Table 2-2)

Examples				2-1	2-2	2-3	2-4	2-5
Step (A)	Ion exchanged water		g	3500	3500	3500	3500	3500
	Natural montmorillonite		g	160	160	160		160
	Natural bentonite		g				180	
	A1110		g	30	15	20	30	
	A1230		g			20		45
	PEGDG		g	30	15		30	
	Methylene chloride		mL	14000	14000	14000	14000	
Step (B)	Basal spacing of the silane-treated foliated phyllosilicate in clay dispersion		Å	>100	75	69	>100	>100
	Polymerizable prepolymer	IPC	g	945	945	945	945	945
		TPC	g	235	235	235	235	235
	Methylene chloride		ml					14000
	Bisphenol A		g					1280
	ptBP		g					41
	Step (C)	Bisphenol A		g	1280	1280	1280	1280
ptBP		g	41	41	41	41		
Polymerization method		—	interfacial polycondensation					
Mw			—	58000	58500	57500	57500	57000
Ash content ratio			wt%	6.71	6.70	6.71	7.52	6.72
Average layer thickness			Å	144	214	272	125	286
Maximum layer thickness			Å	478	635	780	450	840
Number of dispersed particles[N]			particles/ wt%·100 μ ²	93	86	63	135	60
Average aspect ratio			—	83	66	51	76	48
Flexural strength			MPa	122	116	112	115	107
Flexural modulus			MPa	4050	3850	3520	3780	3500
Warpage			—	small	small	small	small	small
Anisotropy(*1)			—	0.998	0.989	0.976	0.998	0.968
Center line average roughness			nm	22	40	65	21	80
Transparency(Haze)			%	5.3	5.6	8.5	4.8	9.2

(*1) Linear expansion coefficient along MD direction/
Linear expansion coefficient along TD direction

(Table 2-3)

Comparative Examples		2-1	2-2	2-3	2-4	2-5
Ion exchanged water	g				768	
Natural montmorillonite	g		160	160	256	
A1110	g			30		
PEGDG	g			30		
Methylene chloride	mL	14000	14000	14000		
Polymerizable prepolymer	IPC	g	945	945	945	
	TPC	g	235	235	235	
Bisphenol A	g	1280	1280	1280		
ptBP	g	41	41	41		
PAR	g				3700	2200
Glass fiber T195H	g					240
Production method	—	interfacial polycondensation			fusion kneading	
Mw	—	5800	58500	57500	56000	57500
Ash content ratio	wt%	0.00	6.70	6.70	6.50	9.84
Average layer thickness	Å	Not measured	32,000	35,000	5200	Not measured
Maximum layer thickness	Å	Not measured	900,000	900,000	8500	Not measured
Number of dispersed particles[N]	particles/ wt%-100 μ^2	Not measured	1	1	6	Not measured
Average aspect ratio	—	Not measured	1.5	1.5	5.3	Not measured
Flexural strength	MPa	89	90	90	91	125
Flexural modulus	MPa	2040	2080	2040	2090	4040
Warpage	—	small	medium	medium	medium	large
Anisotropy	—	0.998	0.998	0.998	0.997	0.113
Center line average roughness	nm	20	806	812	437	1506
Transparency(Haze)	%	1.9	36.7	38.9	23.9	45.2

5 In the following examples, the advantages related to the producing method of the polyester resin composition according to the present invention will be described in comparison with comparative examples.

(Example 3-1)

Step (A)

In 3500 g of ion exchanged water, 150 g of natural montmorillonite was added and mixed by agitation for 5 minutes at 5000 rpm using a wet mill by Nippon Seiki K.K. 10 g of A1120 was then added, and by further agitation under the conditions shown in Table 3-1, a silane-treated foliated phyllosilicate-water dispersion containing a silane-treated foliated phyllosilicate and water was prepared. The confirmation of the silane-treated foliated phyllosilicate was performed by measuring the basal spacing of the separated, dried, and ground solid component by SAXS, and by measuring the absorption bands of functional groups originating from the organo-silane compound in the sample washed with THF by FT-IR. The results of this are shown in Table 3-1 (The results of Examples 3-2 to 3-5 are also shown in Table 3-1).

Step (B)

2500 g of DMT, 1600 g of EG, 7.5 g of hindered phenol-type stabilizer (ADEKA Stab A060, made by Asahi Denka Kogyo K.K., hereinafter, referred to as A060), and 0.60 g of titanium tetrabutoxide ($\text{Ti}(\text{OBu})_4$) were charged in a polymerizer, and then agitated for about 3 hours at a reaction temperature of about 140 to 190°C, thereby transesterifying DMT and EG to obtain an oligomer of PET. The logarithmic viscosity of the obtained oligomer was 0.06 (dl/g).

While agitating the system at 180 rpm, the silane-treated foliated phyllosilicate-water dispersion was gradually added, thereby mixing the oligomer and the silane-treated foliated phyllosilicate-water dispersion.

The addition rate was about 1600 g/hour. The evaporating moisture was drawn out of the system.

Step (C)

5 After completing the addition of silane-treated foliated phyllosilicate-water dispersion, the system was gradually heated to 240°C. After confirming that about 70 to 80% of water contained in the added silane-treated foliated phyllosilicate-water dispersion was drawn out of
10 the system, 0.8 g of antimony trioxide (Sb_2O_3) was added, and the temperature was increased to 280°C. After the temperature increase, the pressure in the system was reduced (0.5 to 5.0 torr (0.067 to 0.665 MPa)) and a fusion polycondensation was performed. The polyester resin
15 composition obtained as described above was evaluated. The results are shown in Table 3-2 (The results of Examples 3-2 to 3-5 are also shown in Table 2).

(Example 3-2)

20 Step (A)

A mixed solvent of 1000 g of ion exchanged water, 1000 g of MeOH, and 150 g of natural montmorillonite were mixed by agitation for 10 minutes at 5000 rpm, using a high-speed agitating homogenizer (Nippon Seiki K.K.). Then,
25 1500 g of ion exchanged water was added, and the mixture was further agitated for 15 minutes at 5000 rpm using a wet mill (Nippon Seiki K.K.). 10 g of A1120 was added thereafter, and the mixture was further agitated under the conditions shown in Table 3-1, whereby a silane-treated
30 foliated phyllosilicate-water dispersion which contains a silane-treated foliated phyllosilicate and water was prepared.

Steps (B) and (C) were conducted in a similar manner to those in Example 3-1, whereby a polyester resin composition was obtained and evaluated.

5 (Example 3-3)

Step(A)

2000 g of ion exchanged water and 150 g of a swellable mica were agitated for 15 minutes at 5000 rpm, using a wet mill (Nippon Seiki K.K.). 16 g of Al120 was added
10 thereafter, and the mixture was agitated under the condition shown in Table 3-1, whereby a silane-treated foliated phyllosilicate-water dispersion containing a silane-treated foliated phyllosilicate and water was prepared.

15 Steps (B) and (C) were conducted in a similar manner to those in Example 3-1, whereby a polyester resin composition was obtained and evaluated.

(Example 3-4)

20 Step (A)

Example 3-4 was conducted similarly to Example 3-1, except that 15 g of Al230 (treated at pH 3 in advance) was added instead of Al120.

25 Steps (B) and (C) were conducted in a similar manner to those in Example 3-1, whereby a polyester resin composition was obtained and evaluated.

(Example 3-5)

30 Example 3-5 was conducted similarly to Example 3-1, except that 18 g of Al174 (treated at pH 3 in advance) was added instead of Al120.

Steps (B) and (C) were conducted in a similar manner to those in Example 3-1, whereby a polyester resin composition was obtained and evaluated.

5 (Comparative Example 3-1)

10 10 g of Al120 was directly sprayed to 150 g of natural montmorillonite using a sprayer, and then by mixing for an hour, the montmorillonite was treated with silane. The basal spacing of the silane-treated montmorillonite was 13 Å. This montmorillonite was washed with THF and then subjected to FT-IR measurement. As a result, the absorption bands originating from primary amino group, secondary amino group, and methylene group were observed.

15 DMT and EG were transesterified in a manner similar to that in Example 3-1. Then, while agitating at 180 rpm, the above-described silane-treated montmorillonite was gradually added and then 0.60 g of Sb_2O_3 was added. A fusion polycondensation was conducted at a reaction temperature of 270 to 280°C and under reduced pressure (0.8 to 5.0 torr) and the resultant product was evaluated. The results are shown in Table 3-2.

(Comparative Example 3-2)

25 Step (A)

30 A silane-treated foliated phyllosilicate-water dispersion was prepared in a manner similar to that in Example 3-1. 1500 g of EG was then added and mixed sufficiently, and agitated for about 9 hours at a temperature of about 100 to 150°C, thereby evaporating and removing water and preparing a dispersion containing the silane-treated foliated phyllosilicate and EG.

Step (B)

2500 g of DMT, 7.5 g of AO60 and 0.60 g of $\text{Ti}(\text{OBu})_4$ were charged in a polymerizer, and agitated at a temperature of about 145 to 150°C, thereby dissolving DMT. The above dispersion containing the silane-treated foliated phyllosilicate and EG was then continuously added and mixed. The addition rate was about 1600 g/hour.

Step (C)

After completing the addition of clay dispersion, the system was agitated for about 3 hours at 145 to 190°C. After heating the reaction system to 240°C, 0.8 g of Sb_2O_3 was added, and the temperature was further increased to 280°C. After the temperature increase, the pressure in the system was reduced (0.5 to 5.0 torr (0.067 to 0.665 MPa)) and a fusion polycondensation was performed. A resin composition was obtained, which was then evaluated. The results are shown in Table 3-2.

20 (Example 3-6)

Step (A)

A silane-treated foliated phyllosilicate-water dispersion was prepared similarly to Example 3-1.

25 Step (B)

3300 g of BHET was charged in a polymerizer, agitated at 150°C under a dry nitrogen flow, and fused. Then, while agitating at 180 rpm, the silane-treated foliated phyllosilicate-water dispersion was gradually added, whereby BHET and the silane-treated foliated phyllosilicate-water dispersion were mixed. The addition rate was about 1600 g/hour. Evaporating water was drawn out of the system.

Step (C)

After completing the addition of silane-treated foliated phyllosilicate-water dispersion, the system was gradually heated to 240°C. After confirming that about 70 to 80% of water contained in the added silane-treated foliated phyllosilicate-water dispersion was drawn out of the system, 7.5 g of A060 and 0.8 g of Sb₂O₃ were charged, and the temperature was further increased to 280°C. After the temperature increase, the pressure in the system was reduced (0.5 to 5.0 torr (0.067 to 0.665 MPa)) and a fusion polycondensation was performed.

The polyester resin composition obtained as described above was evaluated. The results are shown in Table 3-3.

(Comparative Example 3-3)

A dispersion containing a silane-treated foliated phyllosilicate and EG was prepared in a manner similar to that in Comparative Example 3-2.

Using the above dispersion, a polyester resin composition was obtained in a manner similar to that in Example 3-6, which was then evaluated. The results are shown in Table 3-3.

(Example 3-7)

Step (A)

A silane-treated foliated phyllosilicate-water dispersion was prepared similarly to Example 3-1.

Step (B)

10

15

25

(Comparative Example 3-4)

30

Using the above dispersion, a polyester resin composition was obtained in a manner similar to Example 3-7.

(Example 3-8)

A silane-treated foliated phyllosilicate-water dispersion was prepared similarly to Example 3-1.

2200 g of DMT, 1500 g of 1,4-BD, 7.5 g of AO60 and 0.60 g of $\text{Ti}(\text{OBU})_4$ were charged in a polymerizer, and agitated for about 3 hours at a reaction temperature of about 140 to 180°C, for transesterifying DMT and 1,4-BD, thereby obtaining an oligomer of PBT. The logarithmic viscosity of the obtained oligomer was 0.08 (dl/g).

While agitating the system at 180 rpm, the silane-treated foliated phyllosilicate-water dispersion was gradually added, thereby mixing the oligomer and the silane-treated foliated phyllosilicate-water dispersion. The addition rate was about 1600 g/hour. Evaporating water was drawn out of the system.

25 After completing the addition of silane-treated
foliated phyllosilicate-water dispersion, the system was
gradually heated to 250°C. After confirming that about 70
to 80% of water contained in the added silane-treated
foliated phyllosilicate-water dispersion was drawn out of
30 the system, the temperature was further increased to 270°C.
After the temperature increase, the pressure in the system
was reduced (0.5 to 5.0 torr (0.067 to 0.665 MPa)) and a
fusion polycondensation was performed. The polyester resin

composition obtained as described above was evaluated. The results are shown in Table 3-5.

(Example 3-9)

5 Step (A)

A silane-treated foliated phyllosilicate-water dispersion was prepared similarly to Example 3-5.

10 Steps (B) and (C) were conducted in a similar manner to those in Example 3-8, whereby a polyester resin composition was obtained and evaluated. The results are shown in Table 3-5.

(Comparative Example 3-5)

15 In a manner similar to that in Example 3-8, DMT and 1,4-BD were transesterified. Then, while agitating at 180 rpm, the silane-treated natural montmorillonite, which was prepared in a manner similar to that in Comparative
20 Example 3-1, was gradually added and then fusion polycondensation was performed at a reaction temperature of 270°C and under reduced pressure (0.8 to 5.0 torr (0.106 to 0.665 MPa)), and the resultant sample was evaluated. The results are shown in Table 3-5.

25 (Comparative Example 3-6)

A dispersion containing a silane-treated foliated phyllosilicate and 1,4-BD was prepared in a manner similar to that in Comparative Example 3-2, except that 1500 g of 1,4-BD was used instead of EG.

30 The above-described dispersion was added in a manner similar to that in Example 3-8, whereby a polymerization was performed. The results are shown in Table 3-5.

(Comparative Example 3-7)

2500 g of DMT, 1600 g of EG, 7.5 g of AO60 and 0.60 g of $\text{Ti}(\text{OBu})_4$ were charged in a polymerizer, and agitated for about 3 hours at a reaction temperature of about 150 to 190°C, so as to transesterify DMT and ED. 0.60 g of Sb_2O_3 was added thereafter, and a fusion polycondensation was performed at a reaction temperature of 270 to 280°C and under reduced pressure (0.8 to 5.0 torr (0.106 to 0.665 MPa)), whereby PET resin was obtained and evaluated. The results are shown in Table 3-6.

(Comparative Example 3-8)

2200 g of DMT, 1500 g of 1,4-BD, 7.5 g of AO60 and 0.60 g of $\text{Ti}(\text{OBu})_4$ were charged in a polymerizer, and agitated for about 3 hours at a reaction temperature of about 140 to 180°C, so as to transesterify DMT and 1,4-BD. A fusion polycondensation was performed thereafter at a reaction temperature of 250 to 270°C and under reduced pressure (0.8 to 5.0 torr (0.106 to 0.665 MPa)), whereby PBT resin was obtained and evaluated. The results are shown in Table 3-6.

(Table 3-1)

Examples		3-1	3-2	3-3	3-4	3-5	3-6	3-7	3-8	3-9	3-10
Ion exchanged water MeOH	g	3500	2500	2000	3500	3500	3500	3500	3500	3500	3500
			1000								
		150	150		150	150	150	150	150	150	150
				150							
		10	10	15			10	10	10		10
A1120					15						
A1230											
A174						18				18	
Agitation condition: rotation	rpm	5000	5000	6000	5000	5000	5000	5000	5000	5000	6000
Agitation condition: time	hr	0.75	0.75	1.00	0.75	1.00	0.75	0.75	0.75	1.00	1.00
Basal spacing of the isolated clay composite	Å	26	19	23	24	21	26	26	26	21	26
Functional group measured by FT-IR		primary amino group, secondary amino group, methylene group	primary amino group, secondary amino group, methylene group	primary amino group, secondary amino group, methylene group	ether group, methylene group	methyl group, vinyl group, carbonyl group	primary amino group, secondary amino group, methylene group	primary amino group, secondary amino group, methylene group	primary amino group, secondary amino group, methylene group	methyl group, vinyl group, carbonyl group	primary amino group, secondary amino group, methylene group

(Table 3-2)

		Examples					Comparative Examples	
		3-1	3-2	3-3	3-4	3-5	3-1	3-2
Step	Ion exchanged water MeOH	3500	2500 1000	2000	3500	3500		
(A)	Natural montmorillonite	150	150	150	150	150	150	150
	Swellable mica							
	A1120	10	10	16	15	18	10	10
	A1230							
	A174							
	EG							1500
Step	Polymerizable prepolymer	○	○	○	○	○	○	
	DMT							2500
(B)	addition rate of the clay dispersion	1600	1600	1600	1600	1600	—	1600
Step(C)		fusion polycondensation						
Ash content ratio		5.3	5.4	5.6	5.4	5.4	5.5	5.4
Average layer thickness		125	321	258	168	210	32,000(*2)	135
Maximum layer thickness		410	980	775	467	560	900,000(*3)	450
Number of dispersed particles		108	54	71	103	85	1	100
Aspect ratio		148	67	75	116	98	1.5(*4)	145
Production time	Step(A)	0.83	1.08	1.25	0.83	1.08	1.00	10.15
	Step(B)	4.90	4.90	4.25	4.90	4.90	3.35	4.10
	Step(C)	2.50	2.40	2.50	2.40	2.40	2.50	2.50
	total	8.23	8.38	8.00	8.13	8.38	6.85	16.75
Flexural strength		135	100	110	132	105	97	130
Flexural modulus		5750	5010	5250	5680	5280	3160	5650
HDT		215	195	203	214	205	135	214
Warpage		<0.1	<0.1	<0.1	<0.1	<0.1	impossible to mold	<0.1
Surface appearance (center line roughness)		0.04	0.06	0.06	0.04	0.04	0.806	0.04

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(*1) Polymerizable prepolymer: A prepolymer obtained by transesterifying reaction of 2500 g of DMT and 1600 g of EG

5 (*2) This is represented by the numeral average value of the length of the minor axis of the dispersed particle, since it was not dispersed in a plate shape.

(*3) This is represented by the maximum value of the length of the minor axis of the dispersed particle, since it was not dispersed in a plate shape.

10 (*4) This is represented by ratio of (the length of the major axis)/(the length of the minor axis) of the dispersed particle, since it was not dispersed in a plate shape.

			Example	Comparative Example
			3-6	3-3
Step (A)	Ion exchanged water	g	3500	3500
	Natural montmorillonite		150	150
	A1120		10	10
	EG			1500
Step (B)	Polymerizable prepolymer	(*1)	○	○
	Addition rate of the clay dispersion	g/hour	1600	1600
Step(C)			fusion polycondensation	
Ash content ratio		wt%	5.3	5.4
Average layer thickness		Å	110	135
Maximum layer thickness		Å	385	450
Number of dispersed particles		/wt% · 100μ ²	120	100
Aspect ratio			158	145
Production time	Step(A)	hr	0.83	10.15
	Step(B)		2.15	1.35
	Step(C)		2.50	2.50
	total		5.48	14.00
Flexural strength		MPa	134	130
Flexural modulus		MPa	5860	5800
HDT		°C	215	214
Warpage		mm	<0.1	<0.1
Surface appearance (center line roughness)		μm	0.04	0.04

(*1) Polymerizable prepolymer: Bis-hydroxyethyl terephthalate

(Table 3-4)

			Examples	Comparative Example
			3-7	3-4
Step(A)	Ion exchanged water	g	3500	3500
	Natural montmorillonite		150	150
	A1120		10	10
	EG			1500
Step(B)	Polymerizable prepolymer	(*1)	○	○
	Addition rate of the clay dispersion	g/hour	1600	1600
Step(C)			fusion polycondensation	
Ash content ratio		wt%	5.3	5.4
Average layer thickness		Å	130	135
Maximum layer thickness		Å	450	460
Number of dispersed particles		/wt%·100 μ ²	100	100
Aspect ratio			135	135
Production time	Step(A)	hr	0.83	10.15
	Step(B)		3.30	2.50
	Step(C)		2.50	2.50
	total		6.63	15.15
Flexural strength		MPa	124	120
Flexural modulus		MPa	5560	5460
HDT		°C	215	214
Warpage		mm	<0.1	<0.1
Surface appearance (center line roughness)		μm	0.04	0.04

(*1) Polymerizable prepolymer: A prepolymer obtained by depolymerizing 2500 g of PET with 600 g of EG

(Table 3-5)

			Examples		Comparative Examples	
			3-8	3-9	3-5	3-6
Step (A)	Ion exchanged water	g	3500	3500		3500
	Natural montmorillonite		150	150	150	150
	A1120		10		10	10
	A174			18		
	1,4-BD					1500
Step (B)	Polymerizable prepolymer	(*1)	○	○	○	○
	Addition rate of the clay dispersion	g/hour	1600	1600	—	1600
Step(C)			Fusion polycondensation			
Ash content ratio		wt%	5.3	5.4	5.5	5.4
Average layer thickness		Å	128	220	31,000(*2)	135
Maximum layer thickness		Å	410	570	900,000(*3)	450
Number of dispersed particles		/wt%·100μ ²	112	80	1	100
Aspect ratio			156	95	1.5(*4)	145
Production time	Step(A)	hr	0.83	1.08	1.00	9.10
	Step(B)		4.90	4.90	3.35	4.10
	Step(C)		2.50	2.40	2.50	2.50
	total		8.23	8.38	6.85	15.70
Flexural strength		MPa	125	110	86	124
Flexural modulus		MPa	4010	3880	2650	3990
HDT		°C	198	195	162	197
Warpage		mm	<0.1	<0.1	10.5	<0.1
Surface appearance (center line roughness)		μm	0.04	0.06	0.821	0.04

(*1) Polymerizable prepolymer: A prepolymer obtained by transesterifying reaction of 2200 g of DMT and 1500 g of 1,4-BD

5 (*2) This is represented by the numeral average value of the length of the minor axis of the dispersed particle, since it was not dispersed in a plate shape.

10 (*3) This is represented by the maximum value of the length of the minor axis of the dispersed particle, since it was not dispersed in a plate shape.

(*4) This is represented by ratio of (the length of the major axis)/(the length of the minor axis) of the dispersed

particle, since it was not dispersed in a plate shape.

(Table 3-6)

		Comparative Examples	
		3-7	3-8
		PET	PBT
Average layer thickness	Å	Not measured	
Maximum layer thickness	Å		
Number of dispersed particles	/wt%·100 μ^2		
Aspect ratio			
Flexural strength	MPa	2970	2610
Flexural modulus	MPa	104	85
HDT	°C	140	160
Warpage	mm	impossible to mold	10.9
Surface appearance (center line roughness)	μ m	0.02	0.02

5 In the following Examples, the advantages regarding
the rheology characteristics of the polyester resin
composition according to the present invention are
described in comparison with comparative examples.

10 (Example 4-1)

Step (A)

 In 3000 g of ion exchanged water, 160 g of natural
montmorillonite was added and mixed by agitation for
5 minutes at 5000 rpm, using a wet mill by Nippon Seiki K.K.
15 10 g of A1120 was then added, and by further agitation under
the conditions shown in Table 4-1, a silane-treated
foliated phyllosilicate-water dispersion containing a
silane-treated foliated phyllosilicate and water was
prepared. (The confirmation of silane-treated foliated
20 phyllosilicate was performed by measuring the basal spacing
of the separated, dried, and ground solid component by SAXS,
and by measuring the absorption bands of functional groups

5

10

15

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A mixture solvent of 2000 g of ion exchanged water

and 1000 g of ethylene glycol, and 160 g of natural montmorillonite were mixed by agitation for 30 minutes at 5000 rpm, using a wet mill. 10 g of A1120 was added thereafter, and by a further agitation under the conditions
5 shown in Table 4-1, a silane-treated foliated phyllosilicate-water dispersion containing a silane-treated foliated phyllosilicate and water was prepared.

Steps (B) and (C) were conducted in a similar manner
10 to those in Example 4-1, whereby a polyester resin composition was obtained and evaluated.

(Example 4-3)

Step (A)

15 1200 g of ion exchanged water and 50 g of natural montmorillonite were mixed by agitation for 5 minutes at 5000 rpm, using a wet mill. 3.5 g of A1120 was added thereafter, and by a further agitation under the conditions shown in Table 4-1, a silane-treated foliated
20 phyllosilicate-water dispersion containing a silane-treated foliated phyllosilicate and water was prepared.

Steps (B) and (C) were conducted in a similar manner
to those in Example 4-1, whereby a polyester resin
25 composition was obtained and evaluated.

(Example 4-4)

Example 4-4 was conducted similarly to Example 4-1,
except that 10 g of A1230 was used instead of A1120. A
30 polyester resin composition was obtained and evaluated.

(Example 4-5)

Example 4-5 was conducted similarly to Example 4-1,

(Example 4-6)

3500 g of ion exchanged water and 280 g of natural bentonite were mixed by agitation for 10 minutes at 5000 rpm, using a wet mill. 14 g of Al120 was added thereafter, and by a further agitation under the conditions shown in Table 4-1, a silane-treated foliated phyllosilicate-water dispersion containing a silane-treated foliated phyllosilicate and water was prepared.

(Comparative Example 4-1)

3000 g of BHET, 7.5 g of AO60 and 0.60 g of Sb_2O_3 were added to a reactor, and a fusion polycondensation was performed at a reaction temperature of 270 to 280°C and under reduced pressure (0.8 to 5.0 torr (0.106 to 0.665 MPa)), whereby polyethylene terephthalate resin was polymerized. 2250 g of the obtained polyethylene terephthalate resin and 4.5 g of sodium p-t-butylbenzoate (crystallization nucleating agent) were subjected to fusion kneading using a biaxial extruder (The Nippon Steel Works, Ltd., LABOTEX 30), under the conditions at a set temperature of 260 to 280°C and a rotation of 100 rpm. A polyester resin composition was obtained and it was then evaluated. Under certain injection molding conditions, addition of a nucleating agent for crystallization, which is one of the conventional techniques, did not at all improve the

moldability.

The results of the evaluation are shown in Table 4-3
(The results of Comparative Examples 4-2 to 4-7 are also
5 shown in Table 4-3).

(Comparative Example 4-2)

A polyethylene terephthalate resin was polymerized
so as to obtain a resin composition by a method similar to
10 that in Example 4-1, except that 160 g of natural
montmorillonite was used instead of the silane-treated
foliated phyllosilicate-water dispersion. The obtained
resin composition was then evaluated. Merely by directly
adding natural montmorillonite, the values of η_0 - 3η , $\Delta\eta_0$,
15 and $J_{e0} \cdot \eta_0$ did not fall within a desirable range, since only
large particles of natural montmorillonite having a size
of the order of 1 μm were dispersed. Therefore,
releasability and molding cycle during an injection molding
were not improved at all.

20

(Comparative Example 4-3)

10 g of A1120 was directly sprayed to 160 g of
natural montmorillonite using a sprayer, and then by mixing
for an hour, the montmorillonite was treated, i.e., the clay
25 layers was not exfoliated but treated as the aggregate (this
is referred to as a silane-treated montmorillonite). In the
silane-treated montmorillonite, although absorption bands
originating from primary amino group, secondary amino group,
and methylene group were observed, the basal spacing was
30 13 Å, which is the same as the initial value. This means
that the structure of the silane-treated montmorillonite
is different from that of the silane-treated foliated
phyllosilicate used in the present invention.

A fusion polycondensation was performed so as to obtain a resin composition in a manner similar to that in Example 4-1, except that the above silane-treated montmorillonite was used instead of the silane-treated foliated phyllosilicate-water dispersion. The obtained resin composition was then evaluated. The values of η_0 - 3η , $\Delta\eta_0$, and $J_{90} \cdot \eta_0$ did not fall within a desirable range, since the silane-treated montmorillonite was dispersed as only large particles in a size of the order of 1 μm . Therefore, releasability and molding cycle during an injection molding were not improved at all.

(Comparative Example 4-4)

160 g of natural montmorillonite was added to 3000 g of EG, and agitated for 15 minutes at 5000 rpm by a wet mill. Since no water was used, the basal spacing of the natural montmorillonite hardly expanded and the layers were not exfoliated. Under that state, 10 g of A1120 was added, and further agitated under the same conditions as those in Example 4-1, thereby preparing a mixture. In a sample obtained by separating, drying and grinding the solid components from the mixture, absorption bands originating from primary amino group, secondary amino group, and methylene group were observed. The basal spacing, however, was 15 Å, which was substantially the same as the initial value. This means that the structure is different from the structure of the silane-treated foliated phyllosilicate used in the present invention.

A fusion polycondensation was performed so as to obtain a resin composition in a manner similar to that in Example 4-1, except that the above mixture was used instead

of the silane-treated foliated phyllosilicate-water dispersion. The obtained resin composition was then evaluated. As a result, the values of $\eta_e - 3\eta$, $\Delta\eta_e$, and $J_{e0} \cdot \eta_0$ did not fall within a desirable range, since only large particles in a size of the order of $1 \mu\text{m}$ were dispersed. Therefore, releasability and molding cycle during an injection molding were not improved at all. In addition, due to the large particles, the surface quality was deteriorated.

(Comparative Example 4-5)

160 g of natural montmorillonite was added to 3000 g of EG, and agitated for 15 minutes at 5000 rpm by a wet mill. Since no water was used, the basal spacing of the natural montmorillonite hardly expanded and the layers were not also exfoliated.

The sample obtained by agitating the EG and the natural montmorillonite, 2300 g of DMT, 7.5 g of AO60, 0.65 g of $\text{Ti}(\text{OBu})_4$ were charged in a reactor, and agitated for about 3 hours at a reaction temperature of about 190°C , thereby transesterifying DMT and EG. A fusion polycondensation was then performed under the presence of natural montmorillonite at a reaction temperature of 250 to 270°C and under reduced pressure (0.8 to 5.0 torr (0.106 to 0.665 MPa)), whereby a resin composition was obtained, which was then evaluated. By merely mixing natural montmorillonite and EG and polymerization, the values of $\eta_e - 3\eta$, $\Delta\eta_e$, and $J_{e0} \cdot \eta_0$ did not fall within a desirable range, since only large particles of natural montmorillonite in a size of the order of $1 \mu\text{m}$ were dispersed. Therefore, releasability and molding cycle during an injection molding were not improved at all.

2250 g of polyethylene terephthalate resin (obtained by a manner similar to that in Comparative Example 4-1) and 171 g of silane-treated montmorillonite (obtained by a manner similar to that in Comparative Example 4-3) were subjected to fusion kneading using a biaxial extruder (The Nippon Steel Works, Ltd., LABOTEX 30), under conditions in which the set temperature was 260 to 280°C and the rotation was 100 rpm. A resin composition was obtained and the resin composition was then evaluated. Merely by directly kneading the silane-treated montmorillonite, releasability and molding cycle were not improved at all, since only large particles in a size of the order of 1 μ m were dispersed.

840 g of ion exchanged water and 280 g of natural montmorillonite were mixed while applying ultrasonic wave, whereby the natural montmorillonite was swelled.

2250 g of polyethylene terephthalate resin (obtained by a manner similar to that in Comparative Example 4-1) and the above mixture were subjected to a fusion kneading under conditions of a set temperature of 260 to 280°C and a rotation of 350 rpm, using a biaxial extruder with a diameter of 40 mm (The Nippon Steel Works, Ltd., TEX 44). (Volatile moisture was removed through a vent hole under reduced pressure), thereby obtaining a resin composition, which was then evaluated.

As described above, by fusion-kneading natural montmorillonite swelled with water and a resin, the values

of $\eta_0-3\eta$, $\Delta\eta_0$, and $J_{e0}\cdot\eta_0$ did not fall within a desirable range, since the particles are not dispersed finely and homogeneously. Therefore, releasability and molding cycle during an injection molding were not improved at all.

5

(Table 4-1)

Examples		4-1	4-2	4-3	4-4	4-5	4-6
Ion exchanged water	g	3000	2000	1200	3000	3000	3500
Ethylene glycol			1000				
Natural montmorillonite		160	160	50	160	160	
Natural bentonite							280
A1120		10	10	3.5			14
A1230					10		
A187						10	
Agitation condition: rotation	rpm	5000	5000	5000	6000	6000	5000
Agitation condition: time	hr	1.0	1.5	1.0	2.0	2.0	1.5
Basal spacing of the isolated clay composite	Å	26	20	22	21	19	27
Functional group measured by FT-IR		primary amino group, secondary amino group, methylene group	primary amino group, secondary amino group, methylene group	primary amino group, secondary amino group, methylene group	primary amino group, secondary amino group, methylene group	epoxy group, ether group, methylene group	primary amino group, secondary amino group, methylene group

(Table 4-2)

Examples		4-1	4-2	4-3	4-4	4-5	4-6
Ion exchanged water	g	3000	2000	1200	3000	3000	3500
Ethylene glycol	g		1000				
Natural montmorillonite	g	160	160	50	160	160	
Natural bentonite	g						280
A1120	g	10	10	3.5			14
A1230	g				10		
A187	g					10	
Polymerizable prepolymer(BHET)(*1)	g	3000	3000	3000	3000	3000	3000
Addition rate of water dispersion	g/h	2500	2000	2500	2000	1400	1400
Polymerization		fusion polycondensation					
Logarithmic viscosity	g/dl	0.58	0.60	0.61	0.61	0.59	0.54
Ash content ratio	wt%	6.58	6.57	2.16	6.58	6.65	10.25
$J_{e_0} \cdot \eta_0$	sec.	2.5	1.1	1.0	2.2	2.0	3.2
$\eta_0 - 3\eta$	Pa·s	2477	1135	824	2277	2050	3099
$\Delta \eta_0$	Pa·s	2340	989	756	2200	1980	3125
Releasability							
60°C	mold	○	○	○	○	○	○
80°C		○	△	○	○	○	○
100°C		○	△	○	○	○	○
120°C		○	○	○	○	○	○
Cooling time							
60°C	mold	10	18	15	10	11	8
80°C	sec.	10	22	16	10	11	9
100°C	sec.	10	22	17	10	11	9
120°C	sec.	10	20	15	10	11	8
Center line average roughness	nm	22	85	18	22	22	32
Number of dispersed particles [N]	particles/wt%·100 μ^2	132	30	140	122	115	198
Average aspect ratio	—	143	35	161	133	106	89
Average layer thickness	Å	75	390	70	84	105	60
Maximum layer thickness	Å	300	1350	280	350	350	240

(*1): BHET: Bis-hydroxyethylterephthalate

Comparative Examples		4-1	4-2	4-3	4-4	4-5	4-6	4-7
Ion exchanged water	g							840
Ethylene glycol	g				3000	3000		
Natural montmorillonite	g		160	160	160	160	160	280
A1120	g			10	10		10	
Polymerizable prepolymer(BHET)(*1)	g		3000	3000	3000			
Polymerizable prepolymer(DMT)(*2)	g					2400		
Polyethylene terephthalate (*3)	g	2250					2250	3900
Crystallization nucleating agent(*4)	g	4.5						
Production method		fusion kneading					fusion kneading	

Comparative Examples		4-1	4-2	4-3	4-4	4-5	4-6	4-7
Ion exchanged water	g							840
Ethylene glycol	g				3000	3000		
Natural montmorillonite	g		160	160	160	160	160	280
A1120	g			10	10		10	
Polymerizable prepolymer(BHET)(*1)	g		3000	3000	3000			
Polymerizable prepolymer(DMT)(*2)	g					2400		
Polyethylene terephthalate (*3)	g	2250					2250	3900
Crystallization nucleating agent(*4)	g	4.5						
Production method		fusion kneading					fusion kneading	

(Table 4-3)(continued)

Comparative Examples		4-1	4-2	4-3	4-4	4-5	4-6	4-7
Logarithmic viscosity		0.62	0.62	0.63	0.62	0.63	0.62	0.62
Ash content ratio		0.00	6.57	6.58	6.55	6.57	6.62	6.64
$J_{e_0} \cdot \eta_0$		0.20	0.21	0.21	0.23	0.21	0.20	0.20
$\eta_0 - 3\eta$		175	182	186	185	180	176	185
$\Delta \eta_0$		244	250	248	256	249	228	236
Releasability	mold 60°C	○	×	×	△	△	×	×
	80°C	△	×	×	×	×	×	×
	100°C	×	×	×	×	×	×	×
	120°C	○	×	×	×	×	×	×
Cooling time	mold 60°C	35	impossible to mold	impossible to mold	45	46	impossible to mold	impossible to mold
	80°C	50	impossible to mold	impossible to mold	impossible to mold	impossible to mold	impossible to mold	impossible to mold
	100°C	impossible to mold	impossible to mold	impossible to mold	impossible to mold	impossible to mold	impossible to mold	impossible to mold
	120°C	35	impossible to mold	impossible to mold	impossible to mold	impossible to mold	impossible to mold	impossible to mold
Center line average roughness		20	806	750	668	670	660	668
Number of dispersed particles [N]		Not measured	1	1	3	3	1	10
Average aspect ratio (*5)		Not measured	1.5	1.5	1.6	1.5	1.5	2.5
Average layer thickness (*6)	Å	Not measured	32,000	33,000	9800	9900	30,000	2800
Maximum layer thickness (*7)	Å	Not measured	900,000	930,000	25,000	26,000	900,000	8100

(*1): BHET: Bis-hydroxyethylterephthalate

(*3): Polyethylene terephthalate resin polymerized in a similar manner to that in Comparative Example 1

(*5): This is represented by ratio of (the length of the major axis)/(the length of the minor axis) of the dispersed particle, since it was not dispersed in a plate shape.

(*7) This is represented by the maximum value of the length of the minor axis of the dispersed particle, since it was not dispersed in a plate shape.

INDUSTRIAL APPLICABILITY

CLAIMS

1. A resin composition comprising a resin and a silane-treated foliated phyllosilicate,

5 wherein the resin is selected from the group consisting of polycarbonate, polyarylate, and thermoplastic polyester, and the silane-treated foliated phyllosilicate is prepared by introducing an organo-silane compound represented by a general formula (1):

10 Y_nSiX_{4-n} (1)

 (where n is an integer from 0 to 3; Y is a hydrocarbon group with 1 to 25 carbons; the hydrocarbon group may have a substituent(s); X is a hydrolyzable group or hydroxyl group; n Ys may be the same type or different types; and
15 (4-n) Xs may be the same type or different types) into a swellable silicate, and wherein at least one of the following conditions (a) and (b) is satisfied:

 (a) an average layer thickness of the silane-treated foliated phyllosilicate is 500 Å or less; and

20 (b) [N] value is 30 or more (where the [N] value is defined as the number of particles per a unit weight ratio of the silane-treated foliated phyllosilicate contained in an area of 100 μm^2 of the resin composition) and an average aspect ratio is 10 to 300 (where the average aspect ratio
25 is defined as an average of a ratio of a layer length to a layer thickness of the silane-treated foliated phyllosilicate),

 and wherein in the case where the resin is a thermoplastic polyester, at least one of the following
30 conditions (i) to (iii) is further satisfied:

 (i) a difference ($\eta_e - 3\eta$) between an extensional viscosity η_e and the triple value of a shear viscosity η of the resin composition is 300 Pa·s or more at a temperature

of 280°C and a rate of strain of 100 (1/s);

(iii) a product $J_{e0}\eta_0$ of equilibrium compliance J_{e0} and zero shear viscosity η_0 of the resin composition at a temperature of 280°C is 0.8 seconds or more.

3. A resin composition according to claim 1, wherein the resin is a polyarylate.

4. A resin composition according to claim 1, wherein the resin is a thermoplastic polyester.

6. A resin composition according to claim 1, wherein the average layer thickness of the silane-treated foliated phyllosilicate is 500 Å or less and the maximum layer thickness is 2000 Å or less.

7. A resin composition according to claim 6, wherein the [N] value is 30 or more.

9. A method for producing a resin composition according

to claim 1, comprising the steps of:

(A) preparing a clay dispersion including the silane-treated foliated phyllosilicate and a dispersion medium;

5 (B) mixing a polymerizable prepolymer and the clay dispersion; and

(C) forming the resin by polymerizing the polymerizable prepolymer,

wherein, in the case where the resin is a thermoplastic polyester, the clay dispersion comprises a dispersion medium containing water in the step (A).

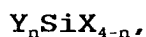
10. A producing method according to claim 9, wherein a
basal spacing of silane-treated foliated phyllosilicate of
15 the clay dispersion prepared in the step (A) is the three
times or more larger than the initial basal spacing of the
swellable silicate.

11. A resin composition according to claim 1, wherein the
20 resin composition is for an injection molding.

12. A resin composition according to claim 11, wherein the resin is a thermoplastic polyester.

ABSTRACT

5 Resin compositions containing polycarbonate, polyarylate
or a thermoplastic polyester resin with a silane-treated
foliated phyllosilicate. The silane-treated foliated
phyllosilicate is prepared by introducing into a swellable
silicate a silane compound represented by the following
10 general formula (1):



wherein n is an integer of 0 to 3; Y is optionally substituted
C₁₋₂₅ hydrocarbon group; and X is a hydrolyzable group or
hydroxy, provided that n Y's and (4-n) X's are the same or
15 different. These resin compositions satisfy at least one
of the following conditions: (a) the silane-treated
foliated phyllosilicate has an average layer thickness of
500 Å or less; and (b) the [N] value is 30 or more and the
average aspect ratio is from 10 to 300. In case of polyester
20 resin compositions, definite conditions on rheological
properties represented by η_0 -3 η , $\Delta\eta_0$ and $J_{e0}\eta_0$ are to be
satisfied too.

Docket No. P9911-187-A010507

ARMSTRONG, WESTERMAN, HATTORI, McLELAND & NAUGHTON, LLP

Declaration for U.S. Patent Application

As a below named inventor, I hereby declare that:

My residence, post office address and citizenship are as stated below next to my name.

I believe I am the original, first and sole inventor (if only one name is listed below) or an original, first and joint inventor (if plural names are listed below) of the subject matter which is claimed and for which a patent is sought on the invention entitled
 (Insert Title) RESIN COMPOSITION AND PROCESS FOR PRODUCING THE SAME
 the specification of which is attached hereto unless the following is checked



was filed on October 12, 1999 as United States Application Number or PCT International Application Number
PCT/JP99/05627 and was amended on _____ (if applicable).

I hereby state that I have reviewed and understand the contents of the above-identified specification, including the claim(s), as amended by any amendment referred to above.

I acknowledge the duty to disclose information which is material to patentability as defined in Title 37, Code of Federal Regulations, ' 1.56.

I hereby claim foreign priority benefits under Title 35, United States Code, §119 (a) - (d) of any foreign application(s) for patent or inventor's certificate listed below and have also identified below any foreign application for patent or inventor's certificate having a filing date before that of the application for which priority is claimed:

(List prior foreign applications. See note A on back of this page)	<u>10-289016</u> (Number)	<u>Japan</u> (Country)	<u>12/October/1998</u> (Day/Month/Year Filed)	Priority Claimed <u>xx</u> Yes ___ No
	<u>10-332951</u> (Number)	<u>Japan</u> (Country)	<u>24/November/1998</u> (Day/Month/Year Filed)	<u>xx</u> Yes ___ No
	<u>11-073225</u> (Number)	<u>Japan</u> (Country)	<u>18/March/1999</u> (Day/Month/Year Filed)	<u>xx</u> Yes ___ No
	<u>11-119075</u> (Number)	<u>Japan</u> (Country)	<u>27/April/1999</u> (Day/Month/Year Filed)	<u>xx</u> Yes ___ No

(See note B on back of this page) ___ See attached list for additional prior foreign applications

I hereby claim the benefit under Title 35, United States Code, § 120 of any United States application(s) listed below and, insofar as the subject matter of each of the claims of this application is not disclosed in the prior United States application in the manner provided by the first paragraph of Title 35, United States Code, § 112, I acknowledge the duty to disclose information which is material to patentability as defined in Title 37, Code of Federal Regulations, § 1.56 which became available between the filing date of the prior application and the national or PCT international filing date of this application.

(List Prior U.S. Applications)

_____ (Appln. Serial No.)	_____ (Filing Date)	_____ (Status: Patented, Pending, Abandoned)
_____ (Appln. Serial No.)	_____ (Filing Date)	_____ (Status: Patented, Pending, Abandoned)
_____ (Appln. Serial No.)	_____ (Filing Date)	_____ (Status: Patented, Pending, Abandoned)

I hereby appoint the following attorney(s) and/or agent(s) to prosecute this application and to transact all business in the Patent and Trademark Office connected therewith:

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I hereby declare that all statements made herein of my own knowledge are true and that all statements made on information and belief are believed to be true; and further that these statements were made with the knowledge that willful false statements and the like so made are punishable by fine or imprisonment, or both, under Title 18 of the United States Code, § 1001 and that such willful false statements may jeopardize the validity of the application or any patent issued thereon.

(See note C
above)

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Residence _____ Citizenship _____
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Full name of sixth inventor (given name, family name) _____
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Residence _____ Citizenship _____
Post Office Address _____

Full name of seventh inventor (given name, family name) _____
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Full name of eighth inventor (given name, family name) _____
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